

1 Title

2 CO₂ plume migration in underground CO₂ storage: the effects of induced hydraulic gradients

3 Authors

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8 Abstract

9 The use of water production as a pressure mitigation tool in the context of CO₂ storage is widely
10 studied but the impact it might have on the migration behaviour of a buoyant CO₂ plume is less well
11 reported. To investigate this further two different scenarios were modelled. In the first, a single
12 water production well was used to draw CO₂ along the strike of an open aquifer with a regional dip.
13 Large rates of water production (5 - 10 times the volume of injected CO₂) were required to achieve
14 only small displacements of the CO₂ plume. The second scenario investigated to what extent an
15 induced hydraulic gradient might spill CO₂ already stored in a structural trap. Here the effects were
16 more pronounced with over 90% of the CO₂ being spilled at a water cycling rate of 10 Mt per year
17 (corresponding to a hydraulic gradient of 1.28 bar/km). The modelling was tested by the real case at
18 Sleipner where CO₂ migration in the Utsira Sand is potentially impacted by water production at the
19 nearby Volve field. Simulations concluded that the CO₂ plume at Sleipner should not be materially
20 affected by water production from Volve and this is supported by the time-lapse seismics.

21 Keywords

22 CO₂ storage; water production; plume steering; Sleipner; Utsira Sand.

23 1. Introduction

24 It is widely recognised that global CO₂ emissions must be drastically reduced to limit the detrimental
25 impact of climate change. One of the main strategies for this is to capture CO₂ at source and store it
26 in deep geological reservoirs. In the context of underground CO₂ storage, water production from
27 wells is cited as a technique for controlling and mitigating the increase in reservoir pressure that
28 might arise from injecting large volumes of CO₂ (Breunig et al., 2013; Buscheck et al., 2012). A
29 secondary application of water production might be to influence the position and/or the migration
30 trajectory of the injected CO₂ plume. So plume steering might be used to prevent the buoyant plume
31 from approaching areas identified as higher risk, such as permeable faults, vulnerable wellbores,
32 areas with less suitable caprock, or even adjacent subsurface operations. Plume steering might also
33 be used to increase the length of the CO₂ migration pathway to increase dissolution and capillary
34 trapping, both of which act to stabilise the CO₂ plume by reducing its mobility and buoyancy, and
35 render the storage less reliant on the caprock as a barrier to leakage.

36 Pressure management by water production during CO₂ injection is mainly to counter induced
37 geomechanical instability, and has been the subject of numerous modelling studies: limiting local
38 pressure increase (Bergmo et al., 2011; Buscheck et al., 2012); reducing the increased pressure
39 spatial footprint (Buscheck et al., 2011; Court et al., 2012); providing an intervention when site
40 pressure exceeds design limits (Le Guenan and Rohmer, 2011); or targeting a specific area which
41 might be vulnerable to increased pressure (Birkholzer et al., 2012). Multiple modelling studies
42 consider the well positioning, well numbers and well production rates required to optimally control
43 pressure increase and maximise CO₂ injectivity and reservoir storage capacity. Pressure reduction is
44 most effective in reservoirs with high permeability, weak permeability heterogeneity and with water
45 production close to the CO₂ injection (Birkholzer et al., 2012; Chadwick et al., 2009; Cihan et al.,
46 2015).

47 Several of these modelling studies cite plume displacement as a possible consequence of pressure
48 management but few studies explore this in greater detail. Buscheck et al. (2012) investigated
49 whether the buoyancy forces which drive CO₂ migration up-dip could be overcome by down-dip
50 water production. The authors found that in a 2D model with a 5.7° slope, producing a volume of
51 water equivalent to that of the injected CO₂, from 10 km down-dip of the CO₂ injection point, was
52 sufficient to prevent CO₂ travelling up-dip, with breakthrough at the production well not occurring
53 for 20-50 years depending on the permeability. Court et al. (2012) simulated CO₂ injection with
54 water production via a 5-spot pattern with four production wells surrounding an injection well. Very
55 little impact on plume position or thickness was found, even on a 50-year timescale, probably
56 because the production wells were tending to pull the CO₂ in mutually cancelling directions.

57 Cameron and Durlofsky (2012) investigated means of maximising residual and dissolution trapping.
58 They produced water from the deepest parts of the reservoir, well away from the CO₂, and
59 reinjected it directly into accumulations of CO₂, vertically above the injection wells. Their strategy
60 was to use periodic water cycling in discrete events optimized for the trapping of CO₂, but the
61 practicalities of injecting water directly into over-pressured CO₂ were not discussed. Similarly,
62 Leonenko and Keith (2008) explored the dissolution potential of water injection. They used the same
63 well for both CO₂ injection and subsequent water reinjection at the top of the reservoir, with water
64 production further afield. Dissolution was enhanced by the water cycling as the plume was forced
65 away from the injection well and into contact with more CO₂-free water in the surrounding reservoir.

66 The potential impact of water production on plume position has yet to be assessed for a range of
67 reservoir types. The main aim of this paper is to investigate the effectiveness of water production as
68 a tool to manipulate the migration trajectory of free CO₂ in storage reservoirs and to quantify the
69 volumes required to have a noticeable impact on plume position. Three numerical fluid flow models
70 are used to examine plume steering in different settings. Firstly a simple box model with a regional
71 dip is used to investigate to what extent water production can perturb a plume of CO₂ away from its
72 buoyancy-driven up-dip pathway. This is relevant to the early stages of a CO₂ storage operation or to
73 storage in an open aquifer. The second model incorporates structural trapping within a small domal
74 feature to quantify the amount of water production (and the resulting hydraulic pressure gradient)
75 that is required to draw CO₂ out of a structural closure. The parameters for both models are based
76 around the Sleipner storage operation, and a third model is used to test the sensitivity of observed
77 plume migration at Sleipner to water production at the Volve Field only 8 km away.

78 2. Planar topseal with a regional dip

79 A simple box model was chosen to examine the influence of water production in the absence of
80 complexities such topseal relief or reservoir heterogeneity. A flat horizon representing an
81 impermeable topseal defines the top of the model, which is then tilted slightly to give a regional dip
82 to the south; the deepest part of the reservoir is at the southern boundary.

83

84 2.1. Model description and parameters

85 The box model extends 7.5 km each way along the strike from the injection well, 7.5 km down-dip
86 (south) and 22.5 km up-dip (where CO₂ is expected to migrate). The thickness of the reservoir is 200
87 m, bounded above and below by impermeable boundaries. Pore-volume multipliers with a value of
88 10⁶ are used on the outer lateral edges of the model to provide approximately hydrostatic boundary
89 conditions, equivalent to a very large uncompartimentalised aquifer. The total pore-volume in the
90 model is 2.4 x 10⁸ km³, easily sufficient to contain realistic quantities of CO₂. This 'open aquifer'
91 configuration prevents boundary effects which might otherwise complicate results.

92 The top of the model centre is placed at a depth of 1000 m below sea level, beneath the
93 impermeable topseal boundary and a regional dip of 0.5 degrees to the south is applied, similar to
94 average dips at the top of the Utsira Sand at Sleipner (Chadwick and Noy 2010).

95 A uniform grid is used with a lateral cell size of 100 m and with the 200 m thick reservoir divided into
96 26 layers, increasing from 0.7 m thick at the top to 20 m at the base. All simulations are run using the
97 Schlumberger ECLIPSE black-oil simulator.

98 Model parameters chosen for this study (Table 1, Figure 1) roughly reflect storage conditions in the
99 Utsira Sand at Sleipner and follow Noy et al. (2012). Average reservoir temperature is taken from
100 Chadwick et al. (2012) and initial pressure is set to hydrostatic.

101

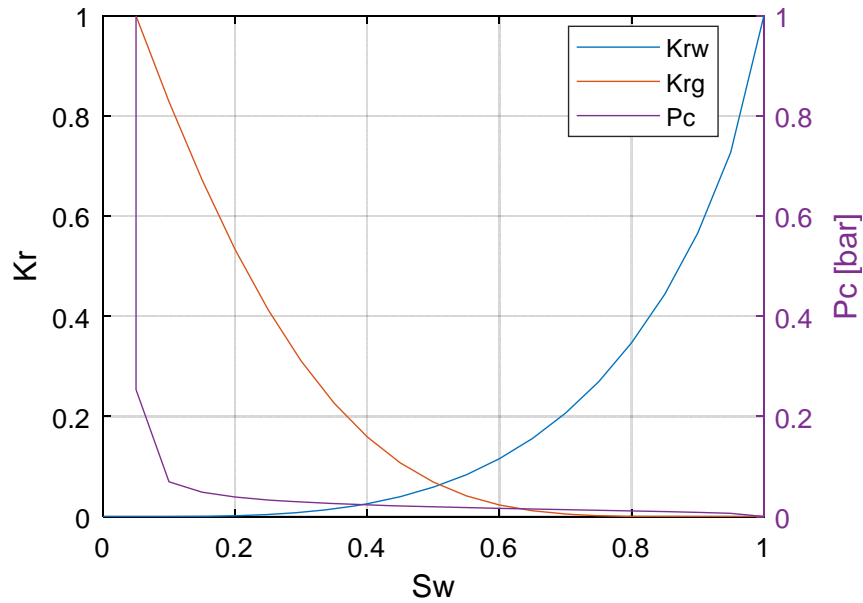
Parameter	Value
Porosity	0.37
Permeability	3040 mD
Permeability anisotropy Kv/Kh	1
Rock compressibility	4.5 x 10 ⁻⁵ bar ⁻¹
Temperature	35 °C
Salinity	32, 000 ppm
CO ₂ injection rate	1 Mt/year

102

103 **Table 1: Parameter values for the base-case**

104

105 A single injection well is positioned centrally along strike in the model, perforated in the deepest cell,
106 with a CO₂ injection rate of 1 Mt/year for a period of 15 years. A single production well positioned 5
107 km to the northwest of the injection well, perforated in the deepest cell only, is used to simulate
108 water extraction from the reservoir for 16 years (one year longer than the injection period). This
109 location, diagonally up-dip of the injection point, is chosen to have a cross-slope influence on the
110 CO₂ plume throughout the production period.



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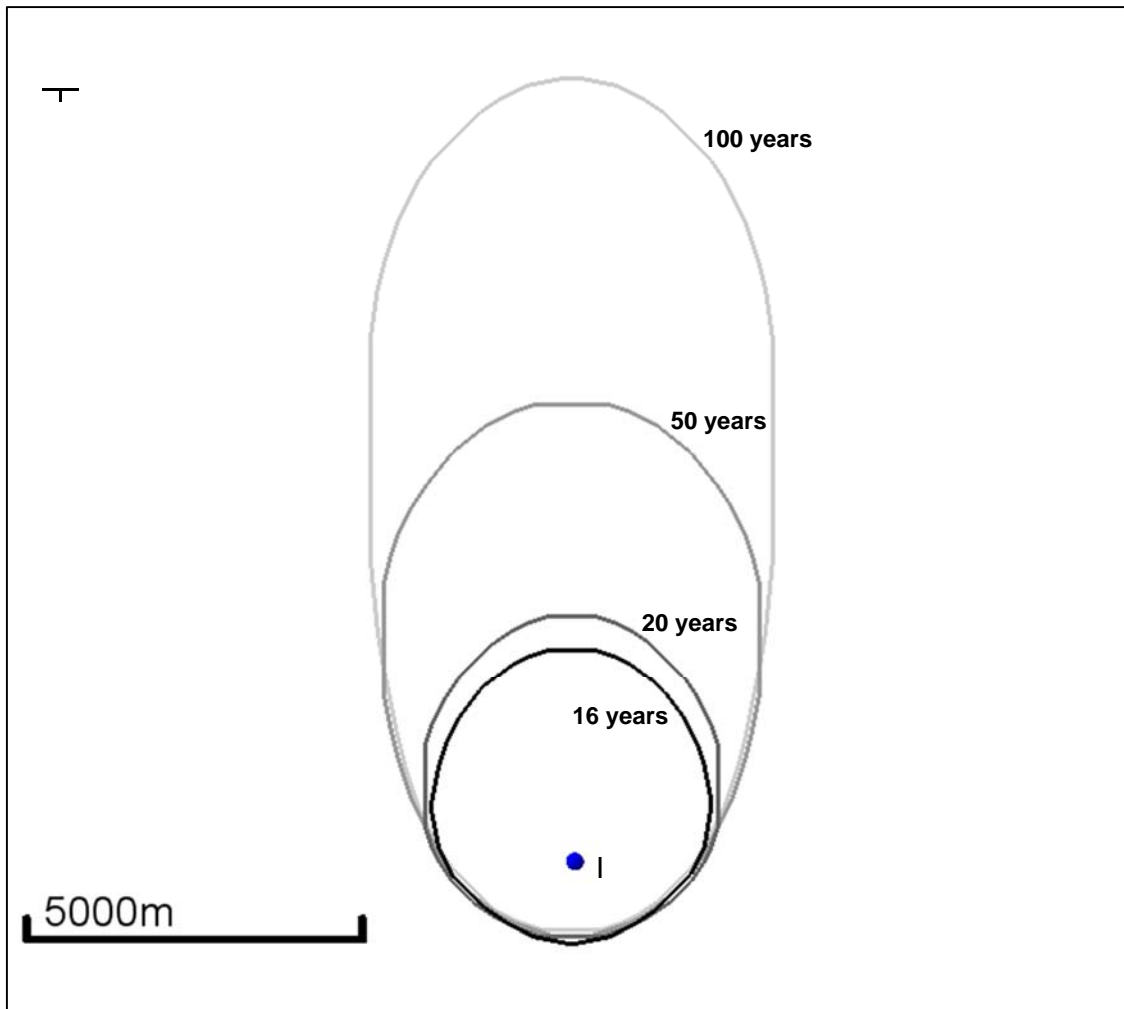
112 **Figure 1: Relative permeability and capillary pressure data used for all simulations, based on the Utsira**
 113 **Sand, taken from Noy et al. (2012).**

114 The rate of water extraction is fixed as a multiple of the volume of CO₂ injected. The volumetric
 115 injection rate, assuming a CO₂ density under the ambient reservoir conditions of 717 kg/m³ (NIST,
 116 2016), was 1.39 x 10⁶ m³/year, so the equivalent mass of water to be extracted is 1.43 Mt/year
 117 (assuming a water density of 1022 kg/m³). This approach of measuring produced water in terms of
 118 injected CO₂ volumes is widely used (Birkholzer et al., 2012; Buscheck et al., 2012; Court, 2011).

119

120 2.2. Plume migration with the base-case flow model

121 A base-case model without any water production was run first, to simulate the purely buoyancy-
 122 driven flow of injected CO₂ (Figure 2). Initially the CO₂ rises to the top of the model, reaching the
 123 topseal after 3 months. The plume then spreads as a thin layer beneath the topseal, initially almost
 124 radially but soon with a marked bias up-dip towards the north, consistent with analytical
 125 approximations of buoyant flow beneath a sloping caprock (Vella and Huppert, 2006). After the end
 126 of injection the CO₂ plume continues to migrate northwards as a thin layer (~20 m thick), leaving
 127 behind a trail of residually trapped CO₂. Residually-trapped CO₂ saturations do not fall below 0.2
 128 since the CO₂ becomes immobile in accordance with the relative permeability curves. The simulation
 129 indicates that, post-injection, the up-dip velocity of the plume stabilises to 0.10 km/year with an R-
 130 squared value of 0.999. For comparison, the Vella and Huppert (2006) analytical solution gives an
 131 up-dip plume velocity in the post-injection phase of 0.11 km/year. Slight discrepancies between the
 132 analytical and numerical solutions can be accounted for by factors such as capillary trapping and
 133 dissolution. Pressure increase due to CO₂ injection is less than 0.5 bar in any given grid cell, giving no
 134 concern with regard to fracture pressure.



135

136 **Figure 2: Base-case plume extents at labelled time steps (after start of injection). CO₂ injection well marked**
 137 **as I. Dip marker indicates the reservoir dip to the south.**

138 2.3. Plume deviation with varying rates of water production

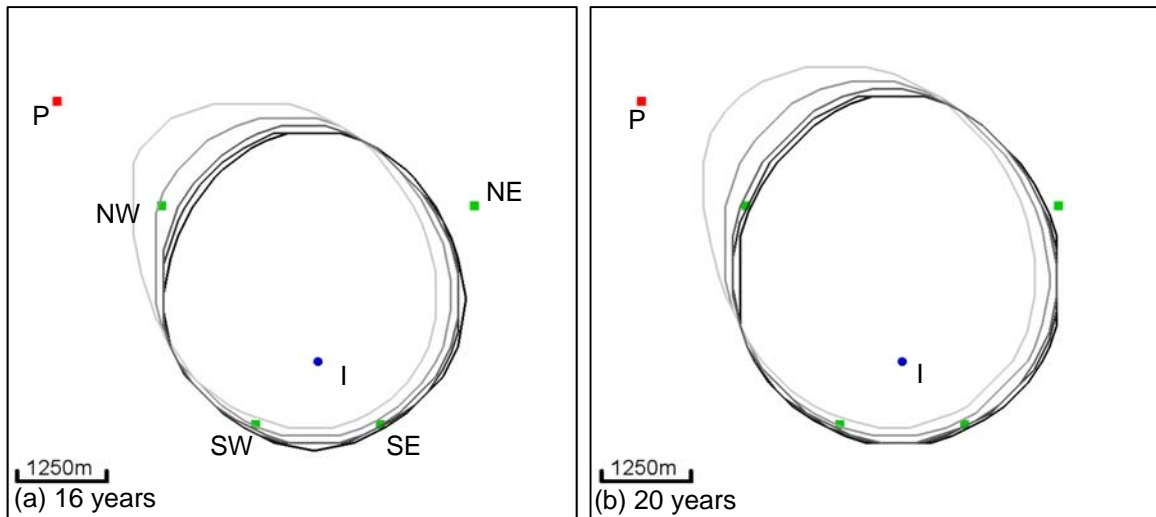
139 A series of simulations was then run with increasing amounts of water production, set as multiples
 140 (0, 1, 2, 5 and 10) of the reservoir volume of injected CO₂ (Figure 3). For the first 20 years of
 141 simulation there is very little impact on the position of the CO₂ plume for volumes of produced
 142 water up to twice the amount of injected CO₂. Effects on plume spreading only become significant
 143 for extracted amounts of water 5 or 10 times the volume of injected CO₂. The impact of water
 144 extraction is most marked at the end of the production period (16 years), with the northwest flank
 145 of the plume displaced by more than a kilometre at higher rates of water production. Subsequent to
 146 the cessation of water production, buoyancy takes over as the principal plume driving force and the
 147 longer-term effect of water production on CO₂ migration is minimal.

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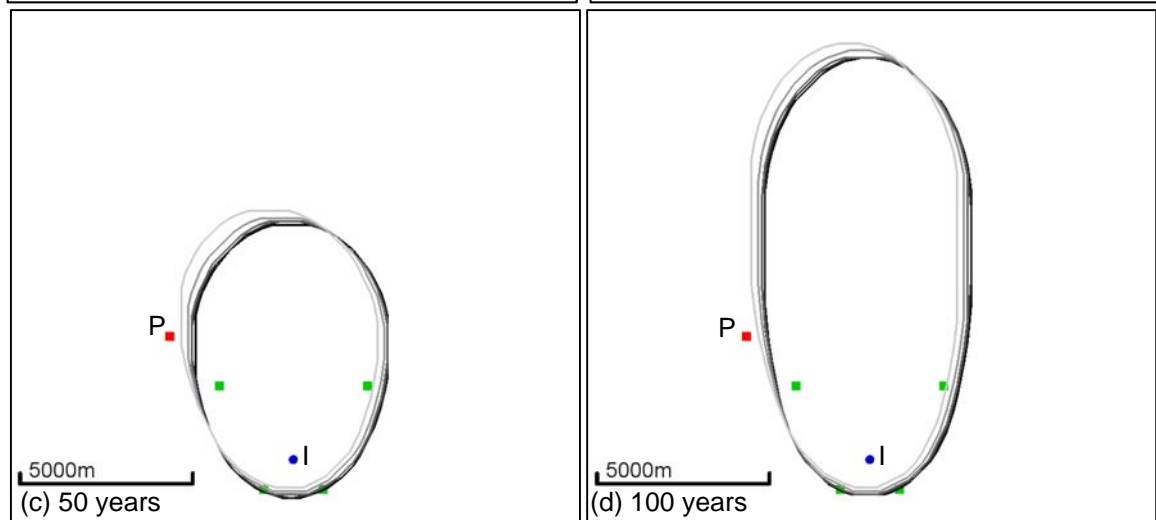
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Figure 3: Plume extents for a range of production volumes (dark grey to light): 0:1 (base-case), 1:1, 2:1, 5:1 and 10:1. Water production well P, sampling points (Figure 4) green. Note change of scale on later plots.

155

2.3.1. Fluid saturation changes

156

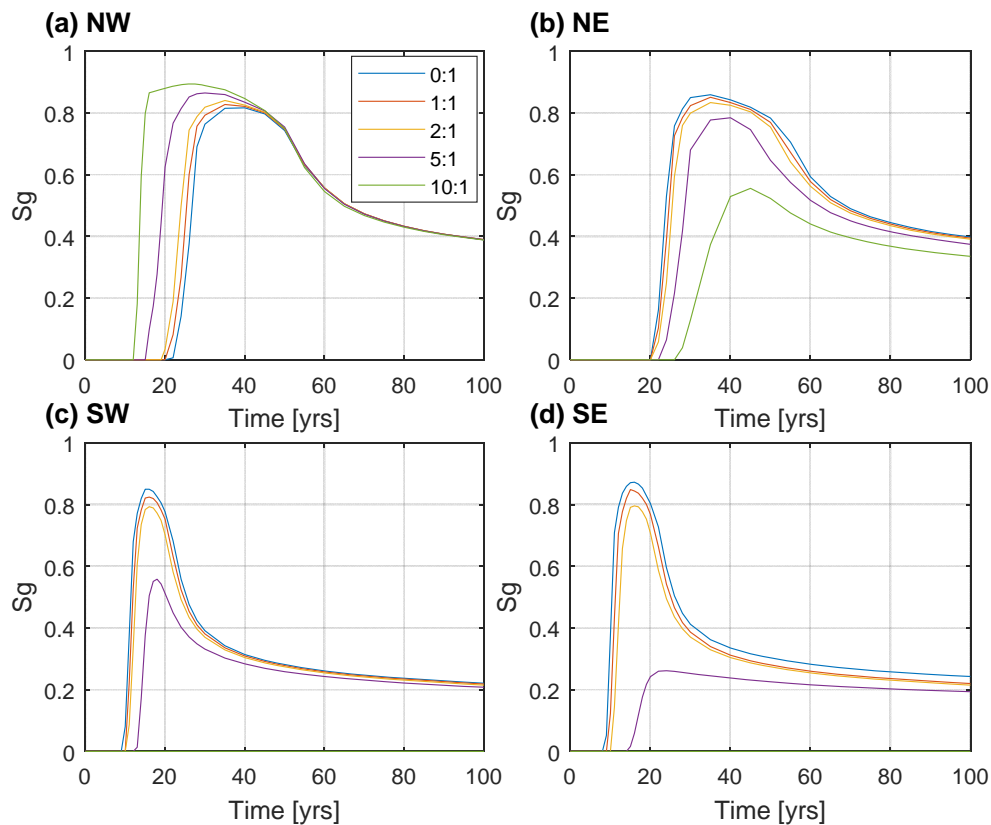
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In order to compare changes in CO₂ saturation associated with the scenarios, four ‘sampling’ locations were chosen to measure gas saturations around the injection well (Figure 3a). The sampling points to the SW and SE of the injection well are 1.2 km away, and those to the NW and NE are 3 km away, the former being closer to the injection point to ensure the presence of CO₂ to measure.



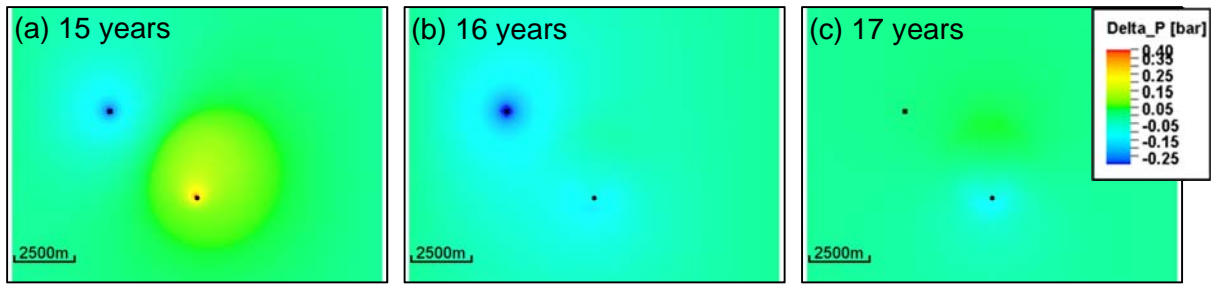
161

162 **Figure 4: Gas saturation in the top cell of the reservoir at the sampling points (for locations see Figure 3).**

163 The larger the water production rate, the greater the impact on the CO₂ plume. The arrival time of
 164 CO₂ at the NW sampling point (located in the direction of the production well) becomes
 165 progressively earlier as larger amounts of water are produced. So without water production, CO₂
 166 arrives after 22 years, whereas with a 10:1 production ratio arrival occurs after only 12 (Figure 4a).
 167 At the NW sampling point CO₂ saturations are always higher for the larger water production ratios.
 168 For the remaining sampling points, NE, SE and SW of the injection well, increased water production
 169 progressively delays arrival of the CO₂, and reduces saturations, to the extent that the 10:1
 170 production ratio completely prevents CO₂ arriving at the SW and SE sample points (Figure 4c, d). This
 171 demonstrates that water production can steer a plume of CO₂ away from specific localities, but the
 172 relative amount of perturbation at the scale of the full plume is quite small (Figure 3). It is noted that
 173 no CO₂ reached the production well in any of these simulations, either in free or dissolved form.

174 2.3.2. Pressure changes

175 The area of low pressure created by water production dissipates radially with distance from the
 176 production well and is superimposed on the pressure increase created by CO₂ injection (Figure 5).
 177 For the first 15 years of the simulation both injection and production wells are operational, and each
 178 creates its own local pressure perturbation. Water production continues for one year beyond
 179 cessation of injection, and the pressure in the reservoir significantly decreases. After the end of
 180 production (16 years) the pressure moves rapidly towards equilibrium because of the high reservoir
 181 permeability and open model boundaries.



182

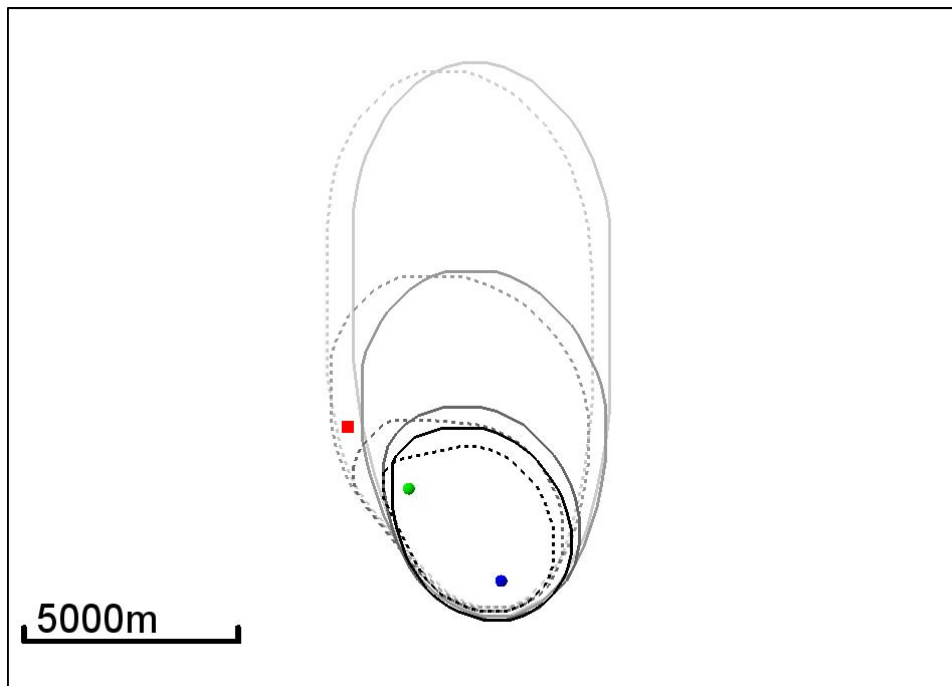
183 **Figure 5: Pressure change (relative to hydrostatic) created by injecting and producing equal volumes of CO₂**
 184 **and water respectively at time steps (a) 15 years i.e. end of injection, (b) 16 years i.e. end of production and**
 185 **(c) 17 years.**

186

187 An additional simulation case was run where water was extracted from the entire reservoir interval,
 188 rather than from just the deepest cell. There was no discernible difference in the location of the CO₂
 189 plume or the hydraulic gradient at the plume. This is because of the large lateral extent of the model
 190 reservoir compared to its thickness.

191 2.4. Plume deviation with a modified production well position

192 In the base-case simulation the water production well was located 5 km away from the injection
 193 point and no CO₂ (free or dissolved) was produced. If the water extraction well were moved closer to
 194 the injection point a larger influence on CO₂ migration would be expected, but at a greater risk of
 195 CO₂ breakthrough. In order to test this trade-off an additional model was run with the production
 196 well positioned 3 km from the injection point (Figure 6).

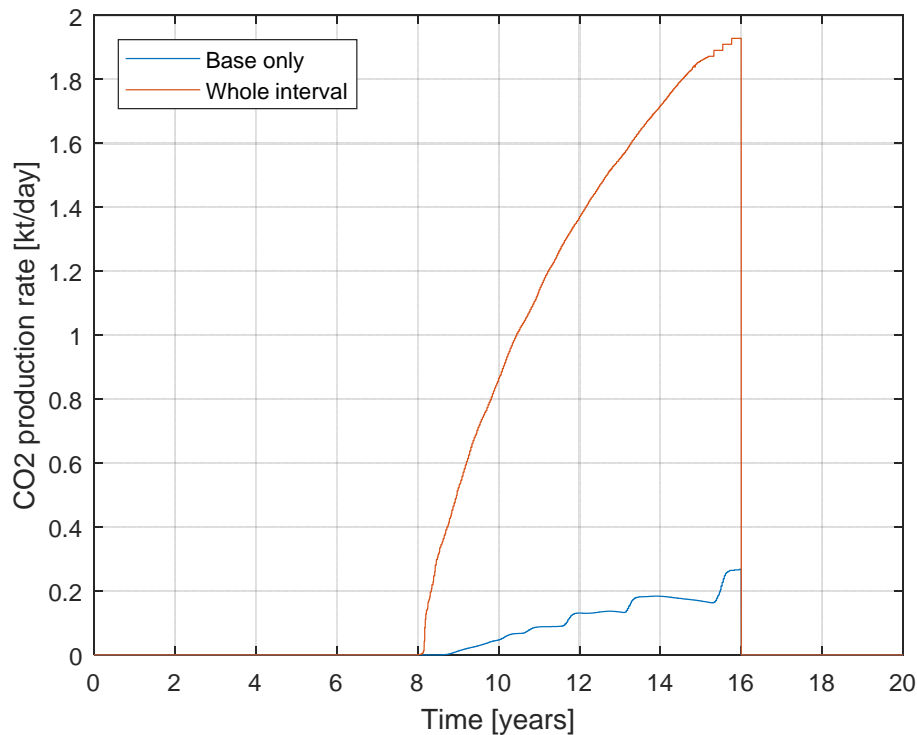


197

198 **Figure 6: A comparison of the plume extent at time steps 16, 20, 50 and 100 years (dark to light) between**
 199 **cases with the production well located 5 km (solid lines, red square) and 3 km (dashed lines, green circle)**
 200 **away from the injection point (blue circle). The extraction ratio is 10:1.**

201 The additional effectiveness of producing water from the nearer location is shown by the long-term
 202 migration path which is displaced a further 500 m to the west. However a consequence of this is that

203 the plume quickly intersected the producing well at 3 km, resulting in the production of CO₂ through
204 the well from about 8 years onwards (Figure 7). The total amount of CO₂ produced from the base cell
205 of the reservoir was 93 kt, 0.6% of the total injected amount. This production of CO₂ undermines the
206 purpose of the CO₂ storage operation. An additional simulation was run where water was extracted
207 over the entire reservoir interval, 3 km from the injection well. In this scenario over 1 Mt of CO₂ was
208 produced (Figure 7). This accounts for 7% of the total injected amount, and highlights the strong
209 benefits of producing water from only the base of the reservoir when there is any risk of the plume
210 reaching the extraction well.



211

212 **Figure 7: Total production rate of CO₂ (free and dissolved) from the production well located 3 km from the**
213 **injector. Production continues for 16 years.**

214 It is clear therefore that optimising the trade-off between obtaining maximum plume steering and
215 preventing premature CO₂ breakthrough is not trivial.

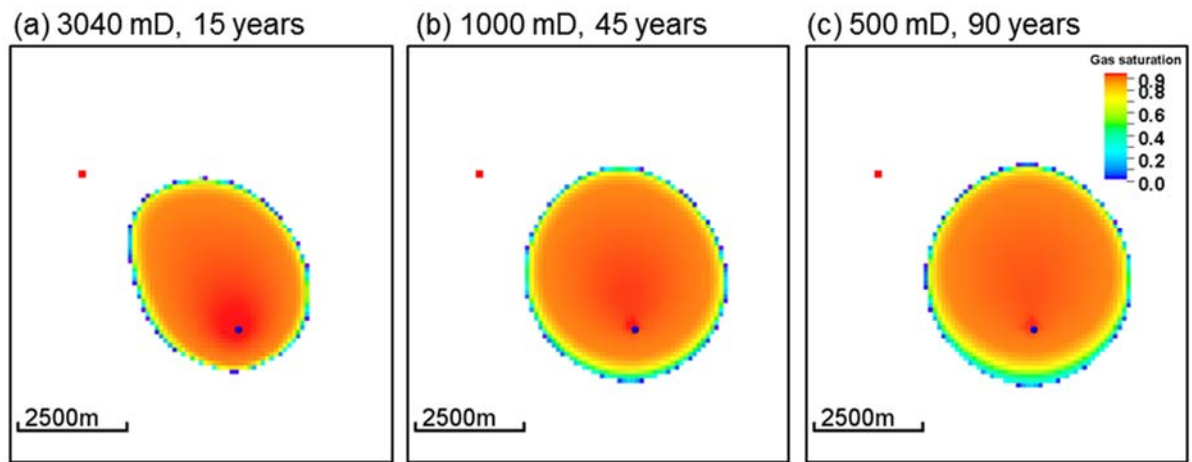
216 2.5. Plume deviation with a different well position relative to the dip

217 A second set of simulations was run with the production well positioned to the SW of the injection
218 point, diagonally down-dip. By the end of the water production stage there is a drawing of the plume
219 by 1 km SW towards the production well for higher production ratios, as noted previously for the
220 NW production well. This enhanced spread of the plume to the SW of the injection well is
221 maintained over the longer term, because of residual saturations of CO₂ becoming fixed due to
222 capillary trapping.

223 2.6. Plume deviation with reduced reservoir permeability

224 To investigate the sensitivity of plume movement to reservoir permeability, two additional scenarios
225 are examined, with permeability reduced to 1000 and 500 mD and the extraction ratio fixed at 10:1
226 (Figure 8). Halving the permeability roughly doubles the time it takes for the plume to migrate a
227 given distance (Figure 8b, c). In consequence, with reduced reservoir permeability, even large

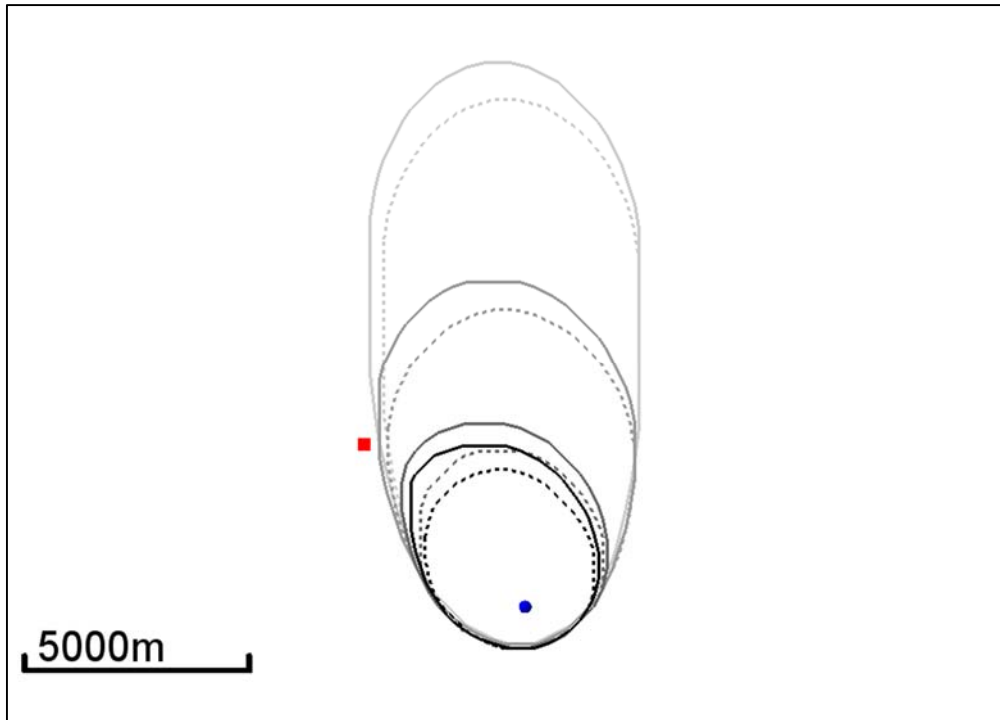
228 amounts of water production have very little impact on plume migration when production is limited
 229 to 16 years (Figure 8b, c). Although the pressure differences are greater when the permeability is
 230 reduced, the low permeability reduces the speed at which CO₂ is able to migrate towards the
 231 production well. So permeability is a limiting factor on the effectiveness of water production as a
 232 tool to influence the migration pathway. Longer times are required for CO₂ to migrate a given
 233 distance in a low permeability reservoir (Figure 8) and it follows that to achieve the same migration
 234 of CO₂ towards a production well the duration of water production would need to be increased.
 235



236
 237 **Figure 8: CO₂ saturation in the top layer of the model with a 10:1 ratio by volume of water production and**
 238 **CO₂ injection. Injection wells are marked with blue circles and production wells are marked with red squares**
 239 **(5 km apart). Water is produced for 16 years in all cases.**

240 2.7. Plume deviation with reduced vertical permeability

241 Permeability anisotropy is common in geological reservoirs, with horizontal fabrics of less permeable
 242 material such as silt and shale restricting vertical permeability. To test the impact of permeability
 243 anisotropy the vertical permeability was reduced by a factor of 10 to 304 mD. This resulted in a
 244 longer time for the plume to reach the top of the reservoir; more than 2 years compared with the 5
 245 months it took with isotropic permeability. In addition, the water production has a smaller effect on
 246 the plume location for the reduced vertical permeability case because the CO₂ was unable to travel
 247 as far in the given 16 year production time period.



248

249 **Figure 9: Comparison of the plume extent with permeability anisotropy $K_v/K_h=1$ (solid lines) and $K_v/K_h=0.1$**
 250 **(dashed lines). The water extraction ratio is 10:1, and displayed time steps are 16, 20, 50 and 100 years (dark**
 251 **to light).**

252 **2.8. Summary**

253 During the water production phase, a noticeable influence on the position of the CO₂ plume is
 254 observed if the volume of water produced significantly exceeds the volume of CO₂ injected (only by
 255 factors of 5x and above). After water production ceases, which for practical reasons is likely to be
 256 roughly when injection ceases, the CO₂ reverts to primarily gravity-driven migration and is free to
 257 continue travelling up-dip, subject to residual trapping and dissolution. Overall on a 100 year time-
 258 scale, the hydraulic gradient caused by producing water up to 10 times the volume of CO₂ injected
 259 has very little impact on the plume position. In this open aquifer configuration, and particularly with
 260 lower permeability reservoirs, water production is not generally effective as a plume steering tool.
 261 There might be an exception if the induced hydraulic gradient forces the plume past a spill-point or
 262 other topographical feature which would change the natural path of the plume.

263 **3. Structural trapping with an induced hydraulic gradient**

264 Buoyant migration of CO₂ beneath a smoothly dipping topseal in a homogeneous reservoir without a
 265 hydraulic gradient is uniformly up-dip with immobilisation of the CO₂ depending entirely on capillary
 266 trapping and/or dissolution. Lateral migration or 'wandering' of the CO₂ plume, either natural or
 267 induced, can have both positive and negative trapping impacts.

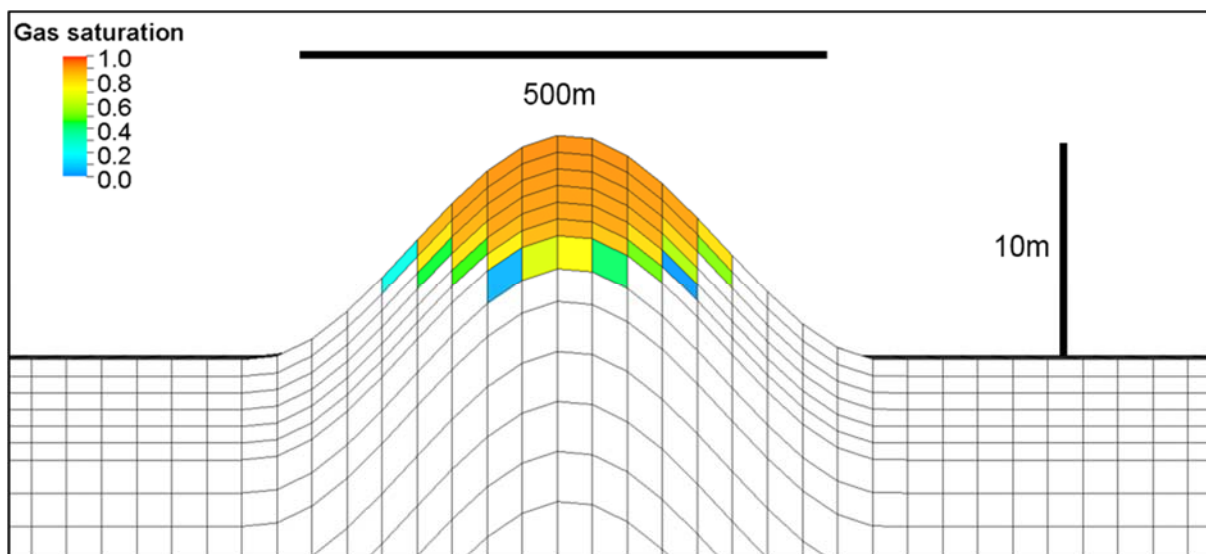
268 On the positive side, topographic 'roughness' on the topseal surface will tend to increase storage
 269 capacity as CO₂ becomes buoyantly trapped in local domal features. Migration meandering produced
 270 by topseal topographic relief or by reservoir heterogeneity will increase the length of migration
 271 pathways and enhance the effect of stabilising processes. On the negative side, plume wandering
 272 would increase its spatial footprint, increasing the potential for reaching leakage pathways and also
 273 increasing the spatial requirements for site monitoring.

274 Lateral pressure gradients in the reservoir have the potential to spill trapped CO₂ from a containing
275 trap. This could either be an unwanted side-effect of producing water for some other purpose (see
276 the Volve example below), or of a naturally occurring hydraulic gradient (groundwater flow).
277 Hydraulic gradients and their impact on hydrocarbon-water contacts were first modelled by Hubbert
278 (1953). Specific sites in the North Sea were later analysed (Dennis et al. 2000; 2005) with hydraulic
279 gradients arising from overpressure in the Central Graben. The amount of tilt on a free-water level is
280 directly related to the density difference between the two fluids. At reservoir conditions the density
281 of CO₂ is similar to that of oil and therefore similar amounts of tilt are possible for naturally occurring
282 hydraulic gradients in CO₂ storage reservoirs (Heinemann et al., 2016).

283 The simulations described below are designed to investigate the interaction of hydraulic gradients
284 and topseal topography by assessing the effect of lateral pressure gradients on the stability of CO₂
285 buoyantly trapped in small structural closures.

286 3.1. Model description and parameters

287 The model extends 11 x 3 km laterally and is 200 m thick with the top located 1000 m below sea-
288 level. A uniform grid is used with a 30 m grid dimension laterally and cell heights increasing from 0.7
289 m at the top to 20 m at the base, giving a total of 146250 cells. A circular structural dome is
290 positioned at the centre of the domain, 250 m in radius, with a range of model scenarios including
291 dome heights of 1, 2, 5, 10 and 20 m (Figure 10). This corresponds to the type of top reservoir
292 topography encountered by the migrating topmost CO₂ layer at Sleipner (Lindeberg et al. 2001). The
293 dome is initially approximately half-filled with CO₂, the total amount of CO₂ being dependent on the
294 size of the dome (Table 2), with an initialisation simulation ensuring equilibrium of the initial
295 conditions.



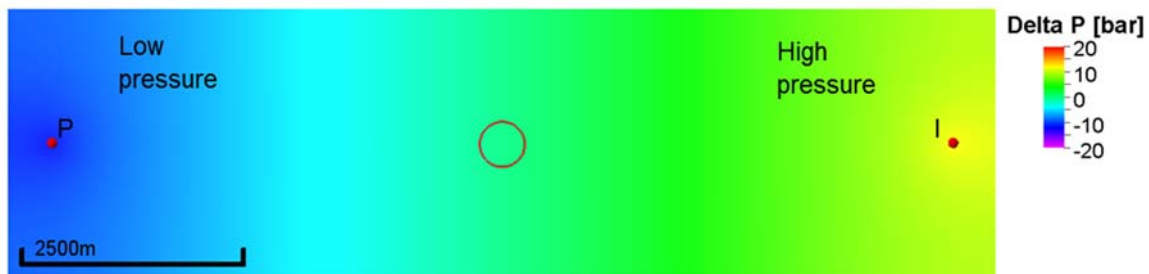
296
297 **Figure 10: A cross-section through part of the model around the dome (10 m high scenario), half-filled with**
298 **CO₂ at the initial conditions. 20x vertical exaggeration.**

Dome height	1 m	2 m	5 m	10 m	20 m
Total initial mass of free CO ₂ (kt)	15.20	19.11	31.51	39.02	99.27
Total initial free CO ₂ (x10 ³ m ³)	21.19	26.65	43.95	54.42	138.45

300

301 **Table 2: Total amounts of free CO₂ initially emplaced in the 10 m structural dome, in units of mass and**
 302 **reservoir volume under average reservoir conditions.**

303 In terms of setting up the hydraulic gradient, a single production well does not really suffice, because
 304 its pressure gradient decreases asymptotically from the well (Figure 5). Here we set up an
 305 analytically more useful pressure distribution of an approximately linear gradient in one dimension.
 306 This is achieved by establishing a two-well water injection-production dipole (Figure 11), with the
 307 dome containing CO₂ situated mid-way between the water wells, 5 km from each. Closed boundaries
 308 are used in this model to maintain the pressure gradient without transverse leakage.



309

310 **Figure 11: The pressure dipole formed by producing 15 Mt/year of water from the well P and injecting 15**
 311 **Mt/year of water into the well I. A structural dome where CO₂ is located has its zero-relief spill-point**
 312 **marked by a red circle (250m radius). Delta P is the increase above hydrostatic pressure.**

313 For each of the simulation cases the dome is initially half-full of CO₂ and water circulation is
 314 simulated for 20 years. A stable pressure gradient, constant in time, is quickly established after
 315 initiation of the water production/injection dipole. After four months of simulation the pressure
 316 reaches a steady state and is constant throughout the depth of the model relative to initial
 317 hydrostatic values (Figure 11). The established hydraulic gradient is directly related to the rate of
 318 water cycling (Table 3), and can approach 2 bar/km for the 15 Mt/year cycling rate. Dennis et al.
 319 (2000) report typical hydraulic gradients of 0.35 bar/km in the North Sea, increasing up to 3 bar/km
 320 for specific fields such as the Pierce Field. The gradient is linear E-W, except for locally around the
 321 wells and within the CO₂ plume, and acts to spill the CO₂ from the dome laterally towards the west.

322

Water cycling (production/injection) rate	Hydraulic pressure gradient
1 Mt/year	0.13 bar/km
5 Mt/year	0.64 bar/km
10 Mt/year	1.28 bar/km
15 Mt/year	1.92 bar/km

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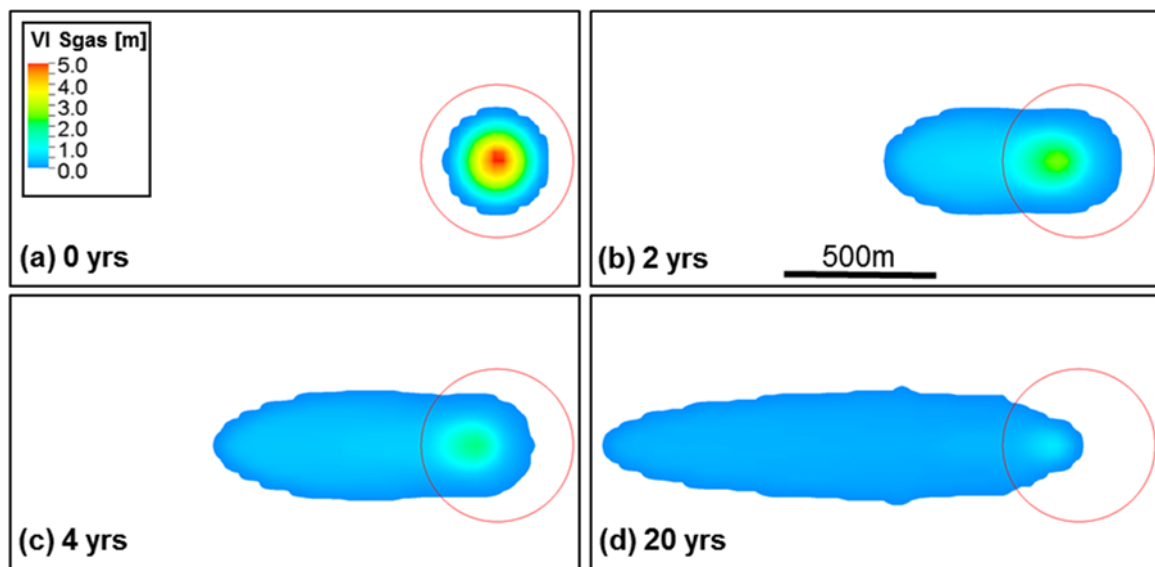
324 **Table 3: Conversion between water injection/production rate and hydraulic pressure gradient.**

325 For comparison with the open aquifer configuration in section 2, an extraction ratio of 1:1 produced
 326 1.42 Mt/year of water.

327 3.2. Model results

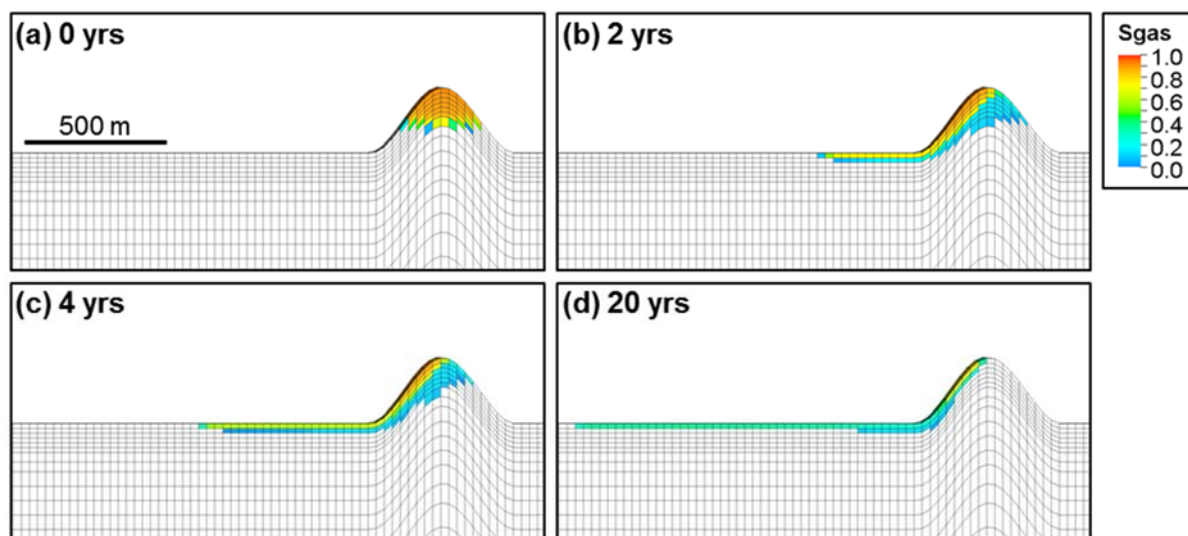
328 The effect of the imposed pressure gradients is to draw the free CO₂ westwards out of the dome,
 329 through its spill-point, towards the low pressure sink (Figures 12 and 13). The amount of CO₂ spilling
 330 is a function of the pressure gradient and the dome elevation (Figure 14). It is noted that no CO₂
 331 reaches the production well (5 km west of the dome) in any of the cases simulated. Dissolution
 332 continues to occur throughout the simulations, decreasing the amount of free CO₂ in the model as
 333 time progresses.

334



335

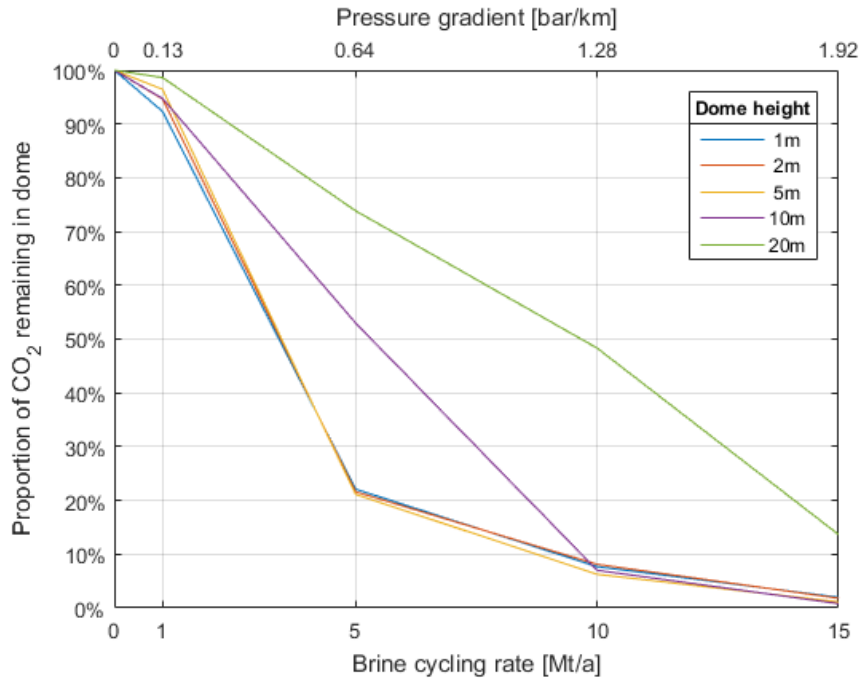
336 Figure 12: Vertically integrated CO₂ saturation (units in metres, i.e. the total thickness of the CO₂ in the
 337 reservoir; to calculate the net CO₂ thickness multiply by the porosity) with a dome height of 10 m and water
 338 cycling rate of 10 Mt/year. The dome spill-point (zero-relief contour) shown in red.



339

340 Figure 13: An E-W cross-section of the free CO₂ saturation through the centre of a dome 10 m high with
 341 water cycling rate 10 Mt/year at labelled time steps, 25x vertical exaggeration.

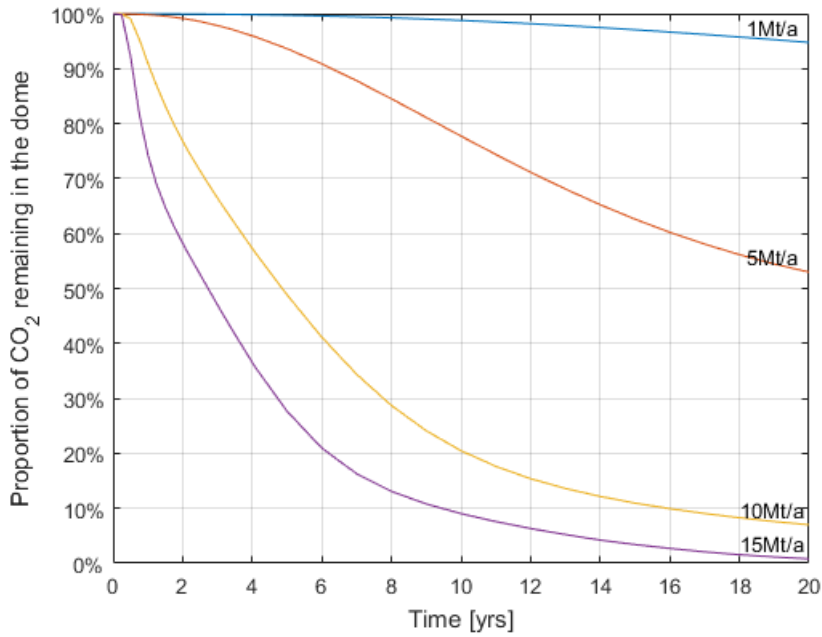
342 The quantities of interest in terms of storage security are the amount of free CO₂ remaining within
 343 the dome (inside the 250 m radius zero-relief contour) relative to the initial total, the farthest
 344 distance travelled by free CO₂ and the proportion of CO₂ dissolving into the formation water. The
 345 latter process is important because dissolved CO₂ is not buoyant and so it markedly increases
 346 security of storage.



347

348 **Figure 14: Proportion of CO₂ (free and dissolved) remaining in the dome after 20 years relative to the initial**
 349 **values (Table 1) against injection/production rate for domes heights 1, 2, 5, 10 and 20m.**

350 Both free and dissolved CO₂ is removed from the structural dome as a result of the imposed pressure
 351 gradients. A water cycling rate of 1 Mt/year over a period of 20 years spills ~7% of the CO₂ from the
 352 1 m dome, but only ~1% of the CO₂ from the 20 m dome (Figure 14). A significant proportion of CO₂
 353 is spilled when the water cycling rate is increased to 5 Mt/year, especially from the smaller domes.
 354 Little difference in the proportion of spilled CO₂ is seen between dome heights of 1 to 5 m, but taller
 355 domes require a larger pressure gradient to spill CO₂ because of the larger depth difference between
 356 the initial CO₂-water contact (CWC) and the spill-point. Cycling rates of 10 Mt/year and above are
 357 sufficient to remove most of the CO₂ from all dome heights over a 20 year period (Figure 14).

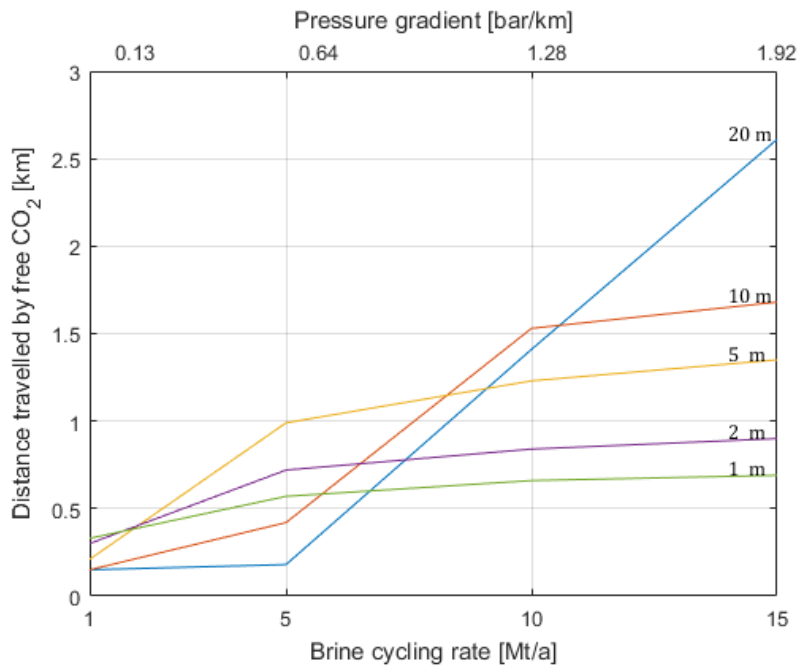


358

359 **Figure 15: Transient proportion of CO₂ (free and dissolved) remaining within a 10 m dome for a series of**
 360 **water cycling rates (labelled).**

361 The rate at which CO₂ is spilled from a structural trap depends on the size of the dome and the water
 362 cycling rate, with for a given dome height, higher cycling rates leading to faster spillage (Figure 15).
 363 For 10 Mt/year of water cycling around half of the CO₂ is removed from a 10 m dome after only 5
 364 years. Although this corresponds to a large-scale water management operation, the 5 year time-
 365 scale is relatively short, indicative of rapid plume response.

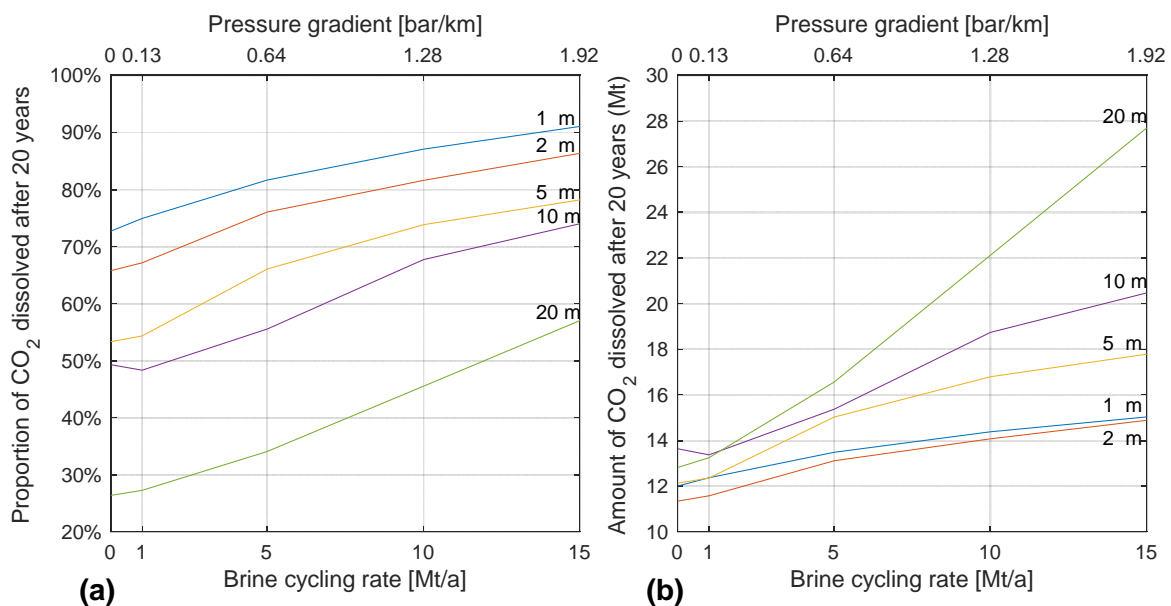
366



367

368 **Figure 16: Graph of maximum distance travelled by free (not dissolved) CO₂ measured from the centre of the**
 369 **dome (250 m radius) after 20 years against water cycling rate for different dome heights (labelled).**

370 The distance migrated by free CO₂ is a good indicator of plume steering potential. For cycling rates of
 371 1 – 2 Mt/year, free CO₂ is not transported past the spill-point of any of the domes more than 2 m
 372 high (Figure 16). Cycling rates of 5 Mt/year produce some spillage from domes up to 10 m tall but do
 373 not tilt the CWC sufficiently (through 10 m of depth change) to spill any CO₂ from the 20 m dome. It
 374 is notable that higher cycling rates (>5 Mt/year) do not produce a proportionate increase in
 375 migration distance for the 1 m and 2 m domes. This is because the amount of free CO₂ initially
 376 available is quite small (Table 2) and dissolution removes most of this as it migrates laterally (see
 377 below). For the taller domes more CO₂ is available, so provided the pressure gradient is sufficient to
 378 bring it to the spill-point, then the free CO₂ plume will travel further overall before dissolution
 379 reduces its size. Provided that the amount of CO₂ is not a limiting factor then the distance travelled is
 380 proportional to the pressure gradient – as evidenced by the 20 m dome scenario (Figure 16).



381

382 **Figure 17: CO₂ dissolution after 20 years plotted against water cycling rate for different dome sizes**
 383 **(labelled). (a) Proportion relative to the amount of CO₂ initially emplaced (b) absolute amount of CO₂.**

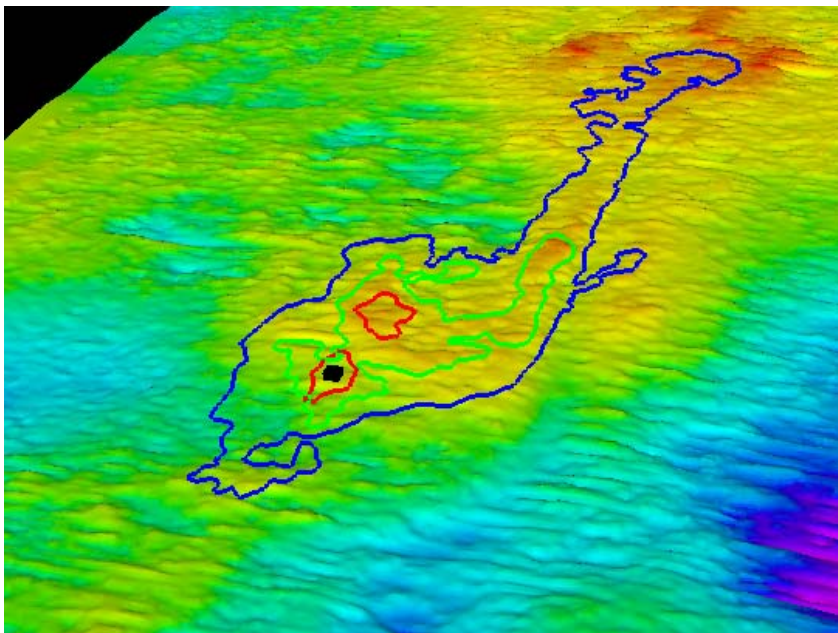
384 The amount of CO₂ dissolving in the different cases can be measured either as a proportion of the
 385 total CO₂ initially within the dome or as an absolute quantity (Figure 17). It is clear that water cycling
 386 strongly enhances CO₂ dissolution, although for the smallest dome (1 m tall), most of the CO₂ (~73%)
 387 dissolves into the water even without water cycling. This is due to the relatively large spatial area of
 388 the CO₂-water contact compared with the small amount of emplaced free CO₂. The more general
 389 tendency for water cycling to increase dissolution has two causes. Firstly water-cycling increases the
 390 plume footprint through spillage and so more free CO₂ is in contact with the surrounding reservoir
 391 water. This is most notable for the 20 m dome where a relatively large migrating plume is
 392 susceptible to dissolution (Figure 17b). A second, more subtle effect is also evident. If we consider
 393 the 20 m dome, for cycling rates up to around 5 Mt/year, no CO₂ is spilled from the dome and there
 394 is no increase in its spatial footprint (Figure 16). Dissolution nevertheless increases from around 26%
 395 with no cycling to ~34% with cycling at 5 Mt/year (Figure 17). This is because with no cycling a
 396 boundary layer of CO₂-saturated water forms beneath the CWC and further dissolution is limited by
 397 diffusion across the boundary layer. With water cycling, CO₂-saturated water beneath the CWC is
 398 continuously swept away to be replaced by CO₂-free water; this allows for much more rapid
 399 diffusion and dissolution at the constantly renewed CO₂-water interface.

400 To conclude, a cycle rate of 5 Mt/year was found sufficient to spill a significant amount (>30%) of
401 CO₂ trapped in domes up to 20 m tall. A sustained pressure gradient of sufficient magnitude was
402 shown to continuously spill CO₂ from a structural trap and, albeit with an idealised flat topseal, to
403 generate a mobile plume migrating more than 2.5 km in 20 years. Increasing the sweep of a CO₂
404 plume by removing it from a structural trap increases the potential for dissolution and residual
405 trapping.

406

407 4. Sleipner and Volve

408 At the Sleipner CO₂ storage project (Baklid et al. 1996), CO₂ is being stored in the Utsira Sand, a large
409 saline aquifer in the Norwegian sector of the North Sea. A multi-layered plume of CO₂ has
410 accumulated in the reservoir since injection commenced in 1996 (e.g. Chadwick et al., 2009, Williams
411 and Chadwick, 2017). The topmost layer of CO₂ in the plume is pooling directly beneath the
412 mudstone topseal and migrating generally towards the north. Time-lapse seismic data show that the
413 CO₂ in this topmost layer is migrating buoyantly via a fill-spill mechanism within small topographic
414 domes and ridges in the topseal, whose relief ranges from just a few metres up to about 20 m
415 (Figure 18).



416

417 **Figure 18: Perspective view (looking north) of the top of the Utsira Sand reservoir at Sleipner showing**
418 **mapped extents from time-lapse seismics of the topmost CO₂ layer in 1999 (red), 2001 (green) and 2006**
419 **(blue). Note the prominent north-trending linear ridge demarcated by the layer extents in 2006. Distance**
420 **from the southern tip of the 2006 polygon to the northern tip is about 3 km. The black marker denotes the**
421 **position of the principle feeder of CO₂ from the deeper plume.**

422

423 An additional model scenario applies the principles of our theoretical study to the Sleipner CO₂
424 storage operation and nearby water production at the Volve oil field, some 8 km to the northwest.
425 Injection of CO₂ at Sleipner is ongoing since 1996 and Volve was operational as an oil field from 2008
426 to 2016. At the peak of production in 2009 Volve produced 3.16 million sm³ oil per year (including
427 small amounts of condensate, NGL and gas, source: Norsk Petroleum). Water was produced from
428 the Utsira Sand and reinjected into the much deeper oil reservoir to provide pressure support for oil

429 recovery. From 2009 to 2015 water production rates were roughly between 1.9 and 3 M sm³/year
430 (Norwegian Petroleum Directorate).

431 To simulate this situation, a numerical model was built with a dome measuring 500 m in diameter
432 and 10 m high containing CO₂ to the spill-point, together with a water production well positioned 8
433 km from the dome centre. The model dimensions are 10 km x 3 km with 30 m grid resolution and
434 200 m reservoir thickness with layering identical to the previous two models in this study. Quasi-
435 infinite pore volume multipliers are applied to the edges of the model to simulate open boundaries
436 with the large surrounding aquifer, consistent with the properties of the Utsira Sand (Chadwick et al.
437 2012). The model top is set at a depth of 1000 m to approximate the Sleipner reservoir pressure and
438 temperature conditions.

439 Water is produced at a rate of 3.2 Mt/year, equivalent to 3 M sm³/year, the higher end of the
440 reported water production range and continues for 40 years. This high value of water production is
441 chosen to give an indication of the maximum impact production at Volve might have on the CO₂ at
442 Sleipner. Close to the production well the induced pressure gradient exceeds 1.5 bar/km, but this
443 reduces to only $\sim 6 \times 10^{-5}$ bar/km in the vicinity of the CO₂ plume. This is much smaller than the
444 hydraulic gradients modelled above (Table 3), and no effect was discernible on modelled CO₂ fluid
445 distributions. For comparison with the open aquifer model, 3.2 Mt/year is equivalent to an
446 extraction ratio of 2.2:1, although in this case the production well is located further away and
447 production continued for a longer time. A second simulation was run with a water production rate of
448 32 Mt/year (ten times the amounts at Volve). This produces a pressure gradient of 15 bar/km
449 around the production well, and $\sim 6 \times 10^{-4}$ bar/km at the CO₂ plume, but still no difference in CO₂
450 distribution is noted, with no detectable lateral spillage from the dome, despite it being filled to the
451 spill-point.

452 We conclude that production from the Volve water production operation is too small and far away
453 to have any detectable effect on the position and migration of the CO₂ plume at Sleipner. This result
454 is supported by the time-lapse 3D seismic data which indicate that in the more distal parts of the
455 topmost layer, CO₂ migration beneath the topseal is governed only by buoyancy-driven migration
456 (Chadwick and Noy, 2010).

457 5. Concluding remarks

458 The effectiveness of water production for influencing the trajectory of a migrating CO₂ plume
459 depends on wider-scale water flow in the reservoir. The pressure gradient of water production from
460 a single modelled well tends to propagate radially and so has a greater impact when channelled in a
461 single direction, such as by flow boundaries. In open homogeneous aquifers the influence of water
462 production can spread over a wide area and even water production rates up to 10 times the volume
463 of injected CO₂ have a very limited impact on a plume only 5 km away, particularly if the natural path
464 of buoyant CO₂ is not altered by the breaching of topographical spill-points. Impact is also limited by
465 the permeability of the reservoir, given realistic time durations for water production.

466 In compartmentalised reservoirs, water production can have a noticeable impact. Cycling 5 Mt/year
467 of water through a water production-injection dipole in a model with closed boundaries had a larger
468 impact on CO₂ migration than producing 10 Mt/year from an open aquifer through a single well. This
469 is because in an open aquifer the surrounding pore space provides recharge for the reservoir,
470 neutralising the pressure sink created by water production. Our simulations with a closed aquifer

471 and water cycling rates of 15 Mt/year showed CO₂ migration distances of up to 2.5 km over a 20-
472 year period.

473 Turning to the possible effects on CO₂ storage at Sleipner of water production at the nearby Volve
474 field, our calculations indicate that in the large, open, Utsira Sand aquifer, the water production is
475 too far from the plume to noticeably influence the migration of CO₂. Only very small hydraulic
476 pressure gradients are induced in the vicinity of the Sleipner plume, insufficient to move CO₂ out of
477 currently occupied topographic traps. This is supported by the time-lapse seismic monitoring results.

478 More generally, the well dipole closed-boundary models showed that induced hydraulic gradients in
479 the range 1 – 2 bar/km are capable of drawing CO₂ laterally out of small topographic traps. These
480 values are in the range of natural head gradients that would result from a reservoir topographic
481 relief of 1000 metres dissipated over a distance of 50 to 100 km. Lateral pressure gradients of this
482 order are not uncommon (e.g. Dennis et al., 2000), so it is clear that CO₂ migration modelling should
483 take into account natural groundwater flows wherever these are likely to be significant, notably in
484 onshore basins with significant relief. Conversely, in situations such as at Sleipner, where there is no
485 hydraulic gradient from a connected onshore aquifer, any 'plume steering' effects due to natural
486 water flow can probably be disregarded.

487 Many of our simulations involved producing a greater volume of water than the volume of CO₂
488 injected with a consequent net fluid/pressure depletion of the site. This might have implications for
489 neighbouring storage sites, connected hydrocarbon fields, mechanical integrity of the reservoir and
490 caprock and, ultimately, the economics of the water production operation.

491 The studies utilised simplified reservoir models with homogeneous properties. The impact of water
492 production will be further complicated by smaller-scale permeability heterogeneity, affecting both
493 the shape as well as the extent of the plume. To apply these principles to a specific storage site
494 would require more detailed modelling incorporating an appropriately detailed level of
495 heterogeneity.

496 The work presented here has the potential to be taken forward in a more generalised analysis, for
497 example by determining a 'critical' value of hydraulic gradient necessary for effective plume
498 steering. There are complexities to this however, in particular reservoir permeability would inversely
499 scale the critical hydraulic gradient, and so generalisation involving the development of a critical
500 gradient - permeability parameter might be the best way forward. Buoyancy of the free CO₂ plume
501 will also have an effect and it might be instructive to compare the relative effects of hydraulic
502 gradient with plume buoyancy forces for different topseal dips.

503

504 Acknowledgements

505 This paper was prepared as part of the research project 'CO₂ Injection and Storage – Short and long-
506 term behaviour at different spatial scales' (EPSRC Grant: EP/K035967/1), with additional support
507 from the UKCCS Research Centre (EPSRC Grant EP/P026214/1). Thanks also to Schlumberger for the
508 use of PETREL and ECLIPSE software. The authors publish with the permission of the Executive
509 Director, BGS (NERC).

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