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1	Influence of Hydraulic Retention Time, Sludge Retention Time and Ozonation
2	on the Removal of Free and Conjugated Estrogens in Japanese Activated Sludge
3	Treatment Plants
4	
5	
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21

Abstract

22 This study describes the occurrence, fate and removal of free estrogens [estrone (E1), 23 17β -estradiol (E2), estriol (E3), 17α -ethynylestradiol (EE2)] and their glucuronide 24 and sulphate conjugates [estrone-3-sulphate (E1-3S), 17β-estradiol-3-sulphate (E2-25 3S), estriol-3-sulphate (E3-3S), estrone-3-glucuronide (E1-3G), 17β-estradiol-3-26 glucuronide (E2-3G) and estriol-3-glucuronide (E3-3G)] in twelve sewage treatment 27 plants (STPs) in Japan. Glucuronide conjugates were only rarely detected in sewage influent and entirely eliminated within the treatment plants. E1 was found at 69 ng/L, 28 29 E2 at 108 ng/L, E1-3S at 18 ng/L and E2-3S at 78 ng/L in sewage influent. Average 30 removal efficiency for E1, E2 and sulphate conjugates was 88, 92 and 93%, 31 respectively following activated sludge treatment. The removal of E1 and E2 was 32 improved with increasing sludge retention time (SRT), with the highest removal 33 typically found from 12 days SRT onwards. The removal of sulphate conjugates was 34 also related to SRT with highest removals found from 8 days SRT onwards. No 35 correlation was found between hydraulic retention time (HRT) and the removal of any 36 of the estrogens. Ozonation (4-7 mg/L) reduced E3 and E2-3S and E3-3S to below 37 detection levels. Overall ozonation reduced the estrogenicity of the effluent as 38 expressed as estradiol equivalents from 8.4 ng/L to 0.7 ng/L. The results suggest 39 adequate river basin management of estrogens in Japan could be accomplished by a 40 mixture of activated sludge plants with long SRT and where necessary the addition of 41 tertiary ozonation.

42

43 Keywords:

Free estrogens; Conjugated estrogens; Activated sludge treatment; Sludge retention
time; Hydraulic retention time; Ozonation

46 **1 INTRODUCTION**

The disruptive impact of steroid estrogens on wild fish and the role played by sewage treatment plants in their discharge is well known [1]. These natural free estrogens have been found to have endocrine disruptive effects on fish even at low ng/L levels [2]. The major source is believed to be the human excretion of free estrogens [2,3]. However, the majority of these estrogens are excreted as conjugates with very limited biological activity [4].

53

54 Steroid estrogens in the free de-conjugated state have been detected in sewage 55 treatment plants (STP) discharge waters worldwide [5-11], implying that de-56 conjugation occurs prior to and/or during wastewater treatment. The conjugated 57 estrogen, depending on the type of attached ester group (glucuronide or sulphate), can 58 potentially de-conjugate back to the active free estrogens [12,13]. For example, 59 elevated levels of estrone (E1) are suspected to arise from transformation of 17β-60 estradiol-3-sulphate (E2-3S) into E1 and 17β-estradiol (E2) in the activated sludge [13]. However, the de-conjugation of glucuronated and sulphated conjugates back into 61 62 their free estrogenic forms occurs at different rates [12,13]. Thus, the de-conjugation 63 process plays a key role in the overall estrogenic potency of sewage effluents and 64 rivers. There are some studies on the fate of conjugates within sewage treatment 65 plants [7,8], but little is known about the influence of different treatment process 66 parameters on their removal.

67

68 Removal of estrogens in sewage treatment is largely a biological process [14,15] and 69 so differences in this part of treatment will have a large effect on the outcome. Such 70 factors include, temperature, dissolved oxygen concentration, substrate loading rate 71 [16] hydraulic retention time (HRT) and sludge retention time (SRT) [17,18]. A 72 minimum sludge retention time of 10 to 12.5 days has been suggested as the period 73 required for the growth of micro-organisms that decompose E2 and E1 [19]. It is not 74 clear; however, to what extent the conditions which favour the removal of free 75 estrogens influence also the fate of the conjugated estrogens. The two groups of 76 compounds have different physico-chemical characteristics with the free estrogens 77 having relatively high octanol-water partition coefficients of 3-4 Log Kow [5], whilst 78 the conjugated estrogens are highly polar [6,7].

79

80 In Japan, particularly in Kinki area (Shiga, Kyoto and Osaka), sewage systems have 81 mostly employed conventional activated sludge process (CAS) in middle and large 82 scale STPs [20]. The CAS is the most widely used process for the treatment of sewage 83 because of its low operation cost and high performance in Japan. However, the 84 operational parameters (SRT, HRT and Dissolved oxygen) and the treatment steps can 85 differ from one plant to another. To the best of our knowledge, this is the first study to report detail exercise on removal of conjugated estrogens in activated sludge as well 86 87 as in advanced wastewater treatment process. Twelve activated sludge treatment 88 processes in Kinki area (Japan) were surveyed to investigate the following:

89

The removal of dissolved natural free and conjugated estrogens within the twelve
 Japanese STPs.

92 2. The effect of HRT and SRT on the removal performance of STPs on free and93 conjugated estrogens.

94 3. Effect of ozonation on free and conjugated estrogen reduction.

95

96 2 MATERIALS AND METHODS

97 2.1 Survey in Japanese STPs

98 Twelve activated sludge treatment systems in Japan (Shiga, Kyoto and Osaka) each 99 with slightly different treatment conditions were investigated. A total of 77 100 wastewater samples (influent=28, secondary effluent=28, final effluent=21) were 101 collected from these STPs. The descriptions of each STP and their operational 102 parameters are given in Table 1. It should be noted that the HRT reported here is the 103 biological step contact time only, not that of the whole process. Out of these twelve 104 plants, three STPs use ozonation as a tertiary treatment process followed the 105 conventional and/or advanced activated sludge process. The ozonation contact time 106 were between 12 to 23 min. Wastewater samples were collected from each STP in 107 three sampling campaigns (November, 2007, November, 2008, and September, 2009). 108 All the plants were sampled in dry weather conditions. The sampling took place at the 109 influent, secondary effluent and effluent stages of the plants concurrently. Population 110 equivalents ranged from 33,900 to 775,500 and the flow rate from 9,500 to 576,265 111 m^{3}/d . The SRT ranges from 3.8 to 22 days with an average of 13 days, whilst the 112 average HRT was 8.7 h (2.4 to 14.1 h).

113

114 Twenty-four hour composite samples were collected using an automatic flow 115 proportional sampler at 4°C. From the sampler, samples were collected in 1 L pre-116 cleaned amber glass bottles and immediately 1 gram ascorbic acid was added to 117 prevent further biodegradation. All samples were transported to the laboratory in a 118 cooler box maintained at 4°C. The filtration and concentration process of the samples 119 were completed within 24 h of sample collection. Sludge samples were not analyzed 120 in this study.

122 **2.2 Sample pre-treatment and chemical analysis**

123 The free and conjugated estrogens; E1, E2, estriol (E3), 17α -ethynylestradiol (EE2), estrone-3-sulphate (E1-3S), E2-3S, estriol-3-sulphate (E3-3S), estrone-3-glucuronide 124 125 (E1-3G), 17β-estradiol-3-glucuronide (E2-3G) and estriol-3-glucuronide (E3-3G) 126 were all obtained from Sigma-Aldrich, Japan. The deuterated standards for each 127 compound were obtained from CDN Isotopes. All the chemicals were analyzed by the 128 ultra-performance liquid chromatography coupled to tandem mass spectrometry 129 (UPLC/MS/MS) [21]. The sample pre-treatment development has been described in 130 some detail previously [21]. Briefly, samples were first filtered with GF/B glass fibre 131 filter (1 µm pore size; Whatman, UK). After adding the appropriate amount of all the 132 deuterated surrogates, solid phase extraction (SPE) with Oasis HLB (200 mg, 6 cc; 30 133 µm partial size, Waters, UK) cartridges was performed. The SPE cartridges were 134 dried for 1 h under the gentle air pressure in a glass manifold. A Sep-Pak Plus NH2 135 (360 mg, aminopropyl, 55–105 µm partial size, waters) cartridge was connected 136 below the dried Oasis HLB cartridge to reduce the effect of sample matrix on ionization. 137

138

139 Free estrogens were eluted first from the cartridge using methanol, followed by 0.5% 140 NH4OH methanol to elute the conjugated estrogens [21]. Chromatographic 141 separations were carried out on a Waters Acquity UPLC system (Milford, MA) using 142 an Acquity BEH C8 column (100 mm, 2.1 mm, 1.7 µm particle size) for free and 143 Acquity BEH C18 column (50 mm, 2.1 mm, 1.7 µm particle size) for conjugated 144 estrogens. Separation was performed with a binary mobile phase (acetonitrile: milli 145 Q) at a flow rate of 0.2 mL/min [21]. UPLC/MS/MS with electrospray ionization in 146 the negative ionization mode was used in this study. The method parameters are

147	shown in the Supporting Information (Table S1). The detection limits of studied
148	estrogens were between 0.2 (sulphate conjugates) and 0.8 ng/L (E3-3G). Recovery
149	rates of each deuterated surrogates were between 65 (E2 in influent) and 108% (E1-3S
150	in influent) (Table S2).
151	
152	(Insert Table 1)
153	
154	2.3 Removal calculations
155	Percentage removal of estrogens during sewage treatment is used as a collective term
156	to describe the disappearance of chemicals from the effluent due to processes such as
157	biodegradation and sorption on sludge. The degree of removal obtained was
158	calculated from the total analyte concentration in raw sewage water (Cin) and effluent
159	(Cout) according to Eq. 1:
160	$\operatorname{Removal}(\%) = \frac{(\operatorname{Cin} - \operatorname{Cout})}{\operatorname{Cin}} \times 100 \tag{1}$
161	Statistical analysis was performed by using commercially available statistical software,
162	Statistica (Statsoft, Tulsa, OK, USA).
163	
164	2.4 Estradiol equivalents (E2 equiv) calculations
165	To address the estrogenic potency for a mixture of natural estrogens (E1 and E2) in
166	terms of E2 equiv was calculated as follows [22].
167	E2 equiv= $[E2] + [EE2] \times 10 + [E1]/3$ (2)
168	These E2 equiv values were used for the investigation of the impact of SRT and
169	ozonation in the removal of estrogenic activity within the STPs.
170	

172 **3 RESULTS AND DISCUSSION**

173 **3.1 Occurrence of free and conjugated estrogens in the wastewater samples**

174 Among the free estrogens, E2 was detected in the range of 5 to 108 ng/L (36 ng/L 175 mean) in influent samples but was detected only in few secondary effluents (up to 9 ng/L) samples. E1 was detected in the range of 11 to 69 ng/L (30 ng/L mean) in 176 177 influent, and 1 to 36 ng/L (3 ng/L mean) in final effluent samples (data not shown). 178 High effluent concentration may reflect de-conjugation of conjugated metabolites 179 during the treatment process[13]. Reported E1 and E2 concentrations are in 180 accordance with previous observations [21,23,24]. E1 values were similar to the 181 previously reported concentrations in Japanese STP, where a range of 66 ng/L 182 (Influent) and 80 ng/L (effluent) was reported. Synthetic estrogen EE2 was never been 183 detected in any sample. This is not unexpected as it is still not a popular method of 184 contraception in Japan [20]. E3 was detected only in influent sample (64 ng/L mean), 185 implying a ready biodegradability during the sewage treatment process.

- 186
- 187

(Insert Figure 1)

188

189 The glucuronide conjugates were found in only two influent samples where E1-3G 190 was found at 3.7 ng/L and E2-3G at 3.5 ng/L concentration. In a previous study, E1-191 3G was detected at 5 ng/L, E2-3G at 4.0 ng/L and E3-3G at 19.0 ng/L in three UK 192 STPs influents [8]. However, D'Ascenzo et al, [25] failed to detect E3-3G, but 193 reported E2-3G at 5.0 ng/L and E1-3G at 4.0 ng/L (mean concentration) in six Italian 194 activated sludge plant influents. Sulphate conjugates were frequently observed in 195 these Japanese STPs influents and secondary effluents (Figure 1) with E2-3S reaching 196 up to 78.0 ng/L (mean concentration 19.4 ng/L) in the influent. E1-3S was detected in influent and few secondary effluent samples at a mean concentration of 8 ng/L (0.8 to
18 ng/L) and 3.4 ng/L (<0.2 to 4.4 ng/L), respectively. This is similar to a previous
survey in an STP in Japan where a range of 7.7 ng/L (E1-3S) and 36.1 ng/L (E3-3S)
in the influent were reported [7]. In an another study in Japan, E1-3S was detected
upto 2.2 ng/L in STP effluent and 0.3 to 0.9 in different river and lake water samples
[26]. E3-3S was never been detected in any effluent samples, however it was detected
upto 19 ng/L in influent samples.

204

3.2 Effect of SRT on estrogen and conjugates removal

206 The E1, E2 and E2 equiv (Eq. 1) removal efficiencies were assessed and compared for 207 each of the STPs in the survey. Results denoted that the longer SRT achieved highest 208 estrogen removal and E1 took longest time to be eliminated completely. Concurrently, 209 there did appear to be a significant relationship (p < 0.05) between SRT and the 210 removal of free estrogens (Figure 2). The highest removal rates could be found from 211 12 d SRT onwards. Mean removal rates of more than 84 and 98% were observed for 212 E1 and E2, respectively, at SRT higher than 12 days. In addition, consistent removal 213 for studied estrogens was observed over 18 days SRT. Previously, more than 90% 214 removal was observed for natural estrogens at SRT of 12-15 days, however in the 215 membrane bioreactors with nitrification and denitrification processes [15]. Whilst, 216 mean removal was 65% for E1 and 85% for E2, at SRT lower than 12 days. This is 217 not to say that SRT periods greater than 12 d guaranteed high removal, but that the 218 highest removal rates were most likely to occur in plants beyond this sludge age. 219 There also seemed to be a significant relationship (p < 0.05) between SRT and removal of the sulphate conjugates, E1-3S ($r^2=0.36$) and E2-3S ($r^2=0.42$). However, in this 220

case the highest removals appeared to be from 8-9 d SRT onwards (more than 99%removal).

223

(Insert Figure 2)

224 A high sludge age will provide a greater opportunity for slow growing 225 microorganisms to establish themselves on the sludge flocs and these have been 226 linked to estrogen biodegradation [15,27]. It seems that species capable of degrading 227 E2 are relatively common in activated sludge [28,29] but this is not the case for E1. 228 However, there is evidence that specialist nitrifying bacteria can degrade E1 and these 229 are favoured by long sludge ages [30,31]. These results imply that increasing sludge 230 age with their attendant bacteria also encourages sulphate conjugate degradation. 231 Recent microcosm studies suggest that a significant proportion of E2-3S can be 232 transformed to the free E1 hormone [13].

233

3.3 Effect of HRT on estrogen and conjugates removal

235 The HRT in the 12 STPs varied from 7 h to 14 h. No relationship between HRT on the 236 removal of the estrogens and their sulphate conjugates was visible (Figure 3). Positive 237 correlation with SRT and not with HRT could be explained by sorption of free 238 estrogens on the sludge. In terms of polarity, free estrogens [log Kow between 2.45] 239 (E3) to 4.01(EE2)] would be considered as moderately hydrophobic compounds [5] 240 and the higher proportion of sorption to sewage particles in wastewater might be 241 expected. However, in case of more hydrophilic sulphate conjugates, bacteria and 242 enzymes can hydrolyze these to yield the free estrogens particularly in activated 243 sludge process [13]. Similar results were reported by Gomes et al, [12], however, 244 using a slightly different media (artificial activated sludge) in a microcosm study.

245

(Insert Figure 3)

246 **3.4 Ozonation and ecotoxicological risk assessment**

247 The STPs; B, C and G having ozonation as a tertiary treatment process were examined 248 in 6 sampling campaigns (Table 2). For these STPs the average E2 equiv removal 249 efficiencies from the influent samples was almost 96% (Table 2). As far as 250 ecotoxicological risk is concern, ozonation reduced the estrogenicity of the effluent as 251 expressed in E2 equiv from 8.4 ng/L to 0.7 ng/L. This indicates that ozonation could 252 reduce the E2 equiv below the threshold (1 ng/L) to cause endocrine disruption to 253 aquatic organisms [22], as 1 ng/L E2 equiv level in the UK is taken as a trigger level 254 for vitellogenin (VTG) production in male fish. Except on one occasion (E1-3S, 0.5 255 ng/L), sulphate conjugates were never detected in effluent samples having ozonation 256 as a tertiary treatment. Previously, ozonation has been found extremely efficient at 257 removing estrogens from the wastewater treatment plants [32,33].

- 258
- 259

(Insert Table 2)

260

261 4 CONCLUSIONS

262 Occurrence and removal of the estrogens and their conjugates were investigated in 263 twelve STPs in Japan. This study demonstrated that sulphate conjugates are readily 264 degraded in Japanese STPs with their removal promoted by longer SRT periods. The 265 HRT of an activated sludge plant had no bearing on its estrogen removal efficiency. 266 On a practical level, this survey suggests that where estrogen removal performance is 267 under consideration, then an SRT above 12 d is desirable, with above 18 d being 268 particularly effective. Ozonation has proved to be particularly effective in estrogen 269 removal whilst conventional activated sludge plants being sufficiently effective with 270 longer SRTs.

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 232–238.
- 389

Figure Captions

- 392
- Figure 1 Concentration (mean) of free and conjugated estrogens in 12 activated sludge
 treatment plants in Japan (n=28); error bar shows range of the detection.
- 395
- Figure 2 Correlation plot of SRT against the E1, E2, E2 equiv, E1-3S and E2-3S
- 397 removal for 12 Japanese STPs (n=28).
- 398
- Figure 3 Correlation plot of HRT against the E1, E2, E2 equiv, E1-3S and E2-3S
- 400 removal for 12 Japanese STPs (n=28).

_			1	~	1			/	
	ID	Treatment	Physicochemical	HRT (h)	SRT (Day)	Sampling Time	Flow (m3/d)	Served population	
	A-1	CAS with coagulation	Chlorination	5.6	18.4	2007/11	57.000	99,000	
A	A-2	AO with carrier	Chiorination	2.8	14.2	2008/12	57,000		
в	B-1	Step AO	Oronotion(4.2mg/l)	9.9	22	2007/11	65.210	84.000	
В	B-2	Pure O2	Ozonation(4.3mg/L)	4.6	9.5	2008/11	05,210	04,000	
с		CAS; AO	Ozonation(7.4 mg/L)	9.8	8.3	2007/11 2008/11	92,280	146,500	
	D-1			12.1	19	2000/11			
D	D-2	CAS;AO;A2O;stepAO	Chlorination	11.6	16	2008/11	576,265	775,500	
i i	D-3	· · · · •		9.4	18	2009/9			
E		AO with coagulation	Chlorination	10.9	17	2007/12	50,000	236,000	
		stepAO with coagulation	Chiorination			2008/12			
F		AO with coagulation	Chlorination	14.1	13.1	2007/12	9,500	33,900	
		stepAO with coagulation	Chionnation			2008/12			
G		AO with coagulation		9.4	12	2007/12	200,000	604,000	
		A2O with coagulation	Ozonation			2008/12			
		stepAO with coagulation							
Н		AO with coagulation	Chlorination	9.9	13	2007/12	39,000	110,000	
		stepAO with coagulation				2008/12			
Т		CAS	Chlorination	7.0	16	2008/11	87,140	210,400	
J	J-1	CAS(quasi-AO)	Chlorination(1.4mg/L)	6.5	6.7	2009/9	191,276	263,137	
5	J-2	CAS	Chlorination(2.0mg/L)	7.0	3.8		,		
κ		AO	Chlorination(2.7mg/L)	8.6	5.0	2009/9	160,544	158,018	
L		AO	Chlorination(1.4mg/L)	8.4	6.3	2009/9	135,833	210,108	
		ventional activated sludge							
	= anox	ic/oxic erobic/anoxic/oxic							
		anoxic/oxic/anoxic/oxic							
-									

Table 1 Detailed description of the surveyed STPs in Japan (Kyoto, Shiga and Osaka)

	Sampling		STP B1			STP C	STP C		STP G		
	event	Inf.	S. Eff.	Eff.	Inf.	S. Eff.	Eff.	Inf.	S. Eff.	Eff.	
E2 Eastin	1^{st}	18.4	6.2	1.7	37.5	9.1	0.7	122.1	10.8	1.2	
E2 Equiv	2^{nd}	14.1	10.6	ND	31.3	7.4	ND	93.1	6.1	0.4	
F1 20	1 st	3.2	ND	ND	4.7	ND	ND	11.2	3.2	0.5	
E1-3S	2^{nd}	1.6	ND	ND	5.2	ND	ND	7.8	ND	ND	
F2 20	1 st	1.8	ND	ND	9.2	ND	ND	61.5	0.8	ND	
E2-3S	2^{nd}	2.3	ND	ND	8.3	ND	ND	41.0	0.4	ND	
E2 20	1 st	6.2	ND	ND	17.9	ND	ND	10.9	0.3	ND	
E3-3S	2^{nd}	8.2	ND	ND	18.7	ND	ND	9.2	0.3	ND	

Table 2 Estradiol equivalent (E2 equiv) and sulphate conjugates concentrations (ng/L) in sewage treatment plants samples having ozonation process as a tertiary treatment.

ND= Not Detected; Inf.= Influent; S. Eff.= Secondary Effluent; Eff.= Effluent

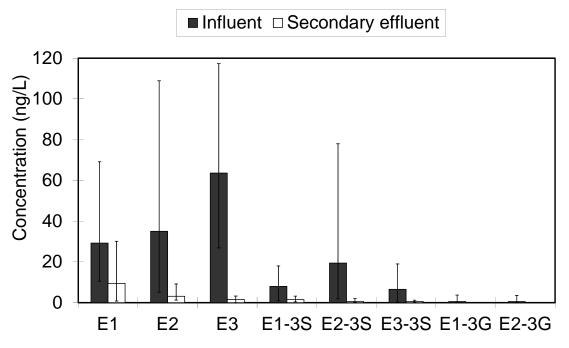


Figure 1 Mean concentration of free and conjugated estrogens in 12 activated sludge treatment plants in Japan (n=28); error bar shows range of the detection.

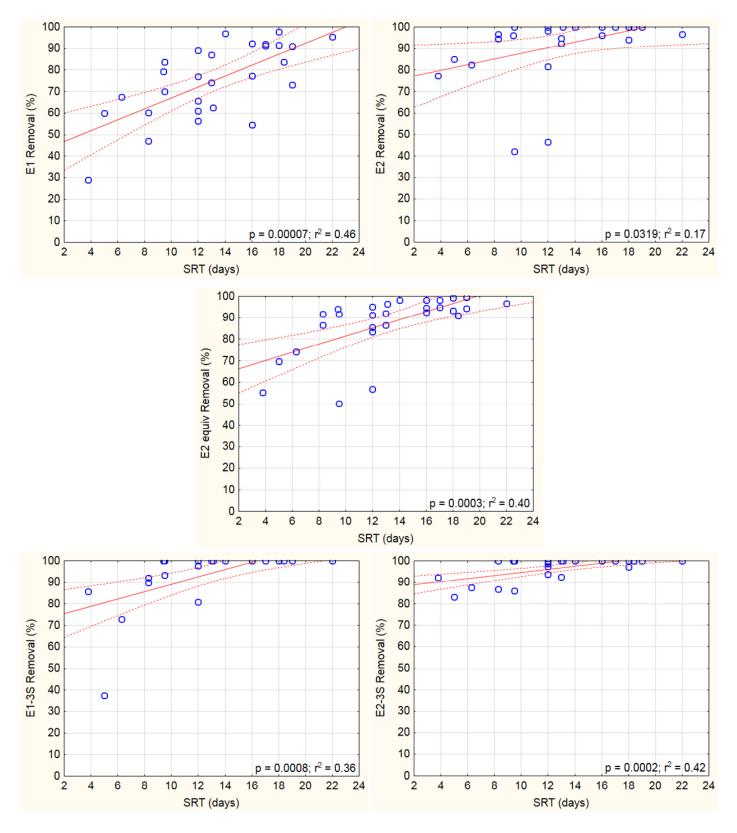


Figure 2 Correlation plot of SRT against the E1, E2, E2 equiv, E1-3S and E2-3S removal for 12 Japanese STPs (n=28).

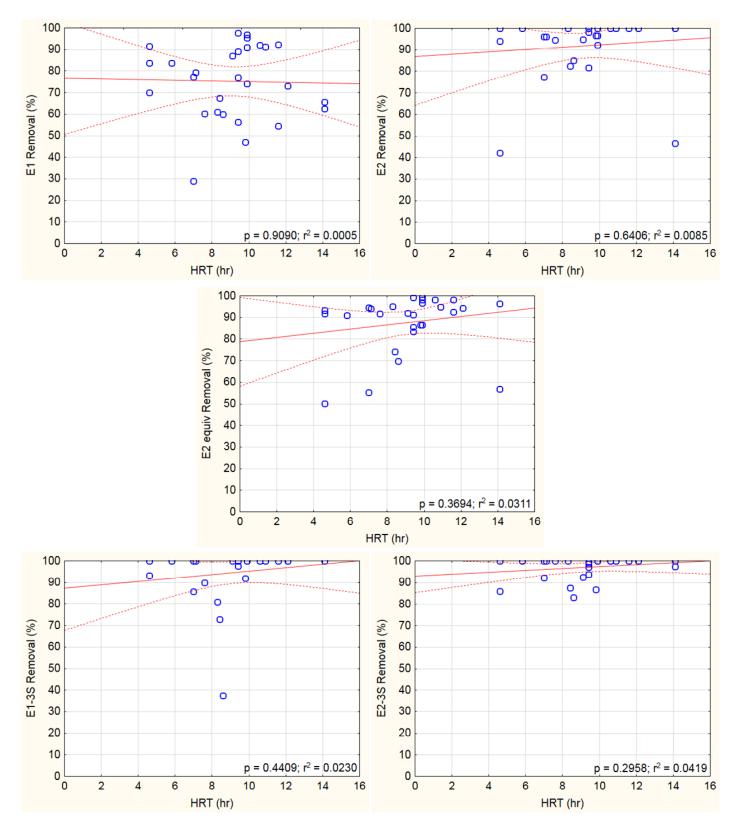


Figure 3 Correlation plot of HRT against the E1, E2, E2 equiv, E1-3S and E2-3S removal for 12 Japanese STPs (n=28).