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28 **Keywords: biofilters, biofiltration, *Phalaris arundinacea*, allelopathy, cyanobacteria**
29 **removal, *Microcystis* removal**

30 **1. Introduction**

31 Eutrophication affects inland and marine waters worldwide since the boom of intensive
32 agriculture practices after the Second World War with typical manifestations of algal (algae
33 and cyanobacteria) blooms (Le Moal *et al.*, 2019; Qin *et al.*, 2019). Water scarcity leading to
34 shortages of potable water due to climate change is a reality (Flörke *et al.* 2018). Furthermore,
35 toxic algal blooms frequency will continue to increase with rising temperatures due to climate
36 change (Huisman *et al.*, 2018). Not only do algal blooms threaten water quality with significant
37 economic, biologic and public health consequences (Martinez-Hernandez *et al.*, 2009; Hudnell,
38 2010; O’Neil *et al.*, 2014; Ger *et al.*, 2014; Otten and Pearl, 2015) but they can cause significant
39 process disruption and reduce output from water treatment works (WTW) up to 25% by
40 interfering/clogging downstream processes (coagulation, slow sand and rapid gravity
41 filtration).

42 Green technologies are widely used for wastewater and water reuse but are less frequently
43 used to remediate eutrophication in reservoirs used for recreational or drinking water purposes.
44 Field scale biofilters based on plant rhizofiltration of high-surface-area are used to absorb
45 nutrient or metals from waste waters (Dushenkov *et al.*, 1995; Enley and Raskin, 2000). The
46 Living-Filter, a floating constructed treatment wetland, was used in a surface reservoir to
47 successfully reduce algal biomass prior to the treatment works for production of potable water
48 (Castro-Castellon *et al.*, 2016).

49 Bench-scale rhizofiltration studies have been limited to nutrient/metal uptake. Marchand
50 *et al.* (2014) combined plants and biofilms for metal removal using planted and unplanted Bio-
51 rack™ to increase copper uptake rate. Kurzbaum *et al.* (2014) separated the role of the roots
52 and the associated biofilm for the removal of pollutants in a hydroponic system, whilst Weiss

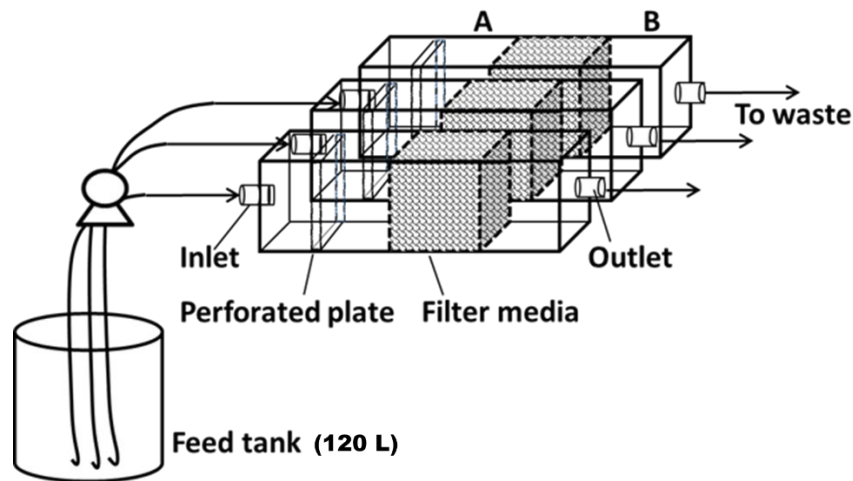
53 *et al.* (2014) used recirculating metal-rich flows to investigate the effect of water flux through
54 hydroponic roots on metal removal. Removal mechanisms of cyanobacteria by biofiltration
55 processes have not been studied before.

56 In this study, filtration units of hydroponically developed *Phalaris arundinacea* (biofilters)
57 and synthetic filters of plastic material were used in a novel set-up under continuous flow
58 conditions to study cyanobacteria (*Microcystis aeruginosa*) cell removal by deposition
59 throughout the filter media (depth filtration). The aim of this study was to determine the
60 interactions of *Microcystis* cells with each type of filter, and to understand how the inflow
61 associated with *Microcystis* cells is processed by the filter media. The outcome of this work
62 will provide insights to improve future designs of field scale Living-Filters promoting the use
63 of green technologies in eutrophic waters.

64 **2. Materials and methods**

65 **2.1 Operational system**

66 An experimental mesocosm was set up to test if hydroponically developed roots can be
67 used in an in-reservoir pre-treatment process for removing cyanobacteria from the inflow prior
68 to the water treatment works. The mesocosm system consisted of triplicate filter units with
69 three types of filter media: one biofilter (i.e. *Phalaris arundinacea* roots) and two synthetic
70 monofilament filters (i.e. plastic three dimensional mesh). In addition, control units with no
71 filter media were included. *Microcystis aeruginosa* 1450/3 was obtained from Culture
72 Collection of Algae and Protozoa (CCAP) (hereafter *Microcystis*) was cultured in
73 photobioreactors and later mixed with dechlorinated water to constitute the feed, which was
74 pumped to the filter and control units. The schematic of the mesocosm set up is displayed in
75 Figure 1.



77 **Figure 1. Schematic of the mesocosm set up showing the feed tank (120L) and only three**
 78 **filtration units (3 L each). Top unit with sampling points, where: A=upstream and**
 79 **B=downstream of the filter; bottom unit showing inlet and outlet of the units, the**
 80 **perforated plate and the position of the filter media.**

81 The filtration units (0.32 m L x 0.104 m W x 0.11m H) were designed in collaboration
 82 with Tuan Ta Ltd., London, UK and made of acrylic transparent material with an internal
 83 perforated plate placed at 0.05 m from the inlet. The units were operated in plug-flow mode,
 84 with water supplied from an air-mixed 120 L high density polyethylene tank through nine lines
 85 of Marprene long life flexible tubing (1.6 x1.6 mm). The inflow was controlled by nine pump
 86 cassettes in three peristaltic pumps (Watson-Marlow Series 500 x2 and a Series 325).

87 **2.2 Hydraulic configuration of the filtration units**

88 Two flow velocities were chosen for running the experiments. A high flow rate (54 ± 3.0
 89 $\text{cm}^3 \text{min}^{-1}$) with a filtration rate of $\sim 0.29 \text{ m h}^{-1}$ was chosen to resemble the range of filtration
 90 rates for slow sand filters ($0.3 - 0.6 \text{ m h}^{-1}$) as slow sand filtration is an effective ecological
 91 process in supply water treatment (Campos *et al.* 2002). A low flow rate ($1.3 \pm 0.2 \text{ cm}^3 \text{min}^{-1}$)
 92 was chosen to investigate whether deposition mechanisms could take place in the filter media.

93 Laminar flow in the system becomes mixed in contact with the filter media. The hydraulic
 94 properties of the system are summarized in Table 1.

95 **Table 1. Hydraulic properties of the filter units**

Experimental flow	Cross Sectional Area (m ²)	Volume (m ³)	V=Q/A (m h ⁻¹)	Q (cm ³ h ⁻¹)	HRT= Vol/Q (s)
Low	1x10 ⁻²	3.3x10 ⁻³	0.005	60	2.008x10 ⁻⁵
High	1x10 ⁻²	3.3x10 ⁻³	0.29	3.3x10 ⁻³	3.3x10 ⁻³

96 V: velocity; Q: discharge; HRT: hydraulic retention time; Vol: volume

97 **2.3 Fluid flow of *Microcystis* cells through biological and synthetic filter media**

98 Three types of filter media were compared: the living roots of hydroponically grown
 99 *Phalaris arundinacea* and two synthetic monofilament fabrics with different packing density
 100 (fabric 1 and fabric 2). The packing density for the filter media was estimated from Equation
 101 (1):

102 Packing density = volume occupied by roots or fabric/ total volume (10 cm³) (1)

103 Stainless steel cages (10 cm³) were made to contain the biofilters and synthetic media, and
 104 empty cages were placed in the control units. The wire diameter was 1.1 mm with an aperture
 105 width of 14 mm.

106 **2.3.1 Biofilters: hydroponic growth of *Phalaris arundinacea***

107 Seeds of *Phalaris arundinacea*, a species from the Poaceae family known as Reed Canary
 108 Grass, were obtained from British Wildflower Plants, Norfolk, UK and cultivated in sterile
 109 coconut coir pellets. After two weeks, the roots of plantlets were rinsed, rolled up individually
 110 in strips of foam and transferred to 50 cm³ Falcon™ tubes. To maximize the production of
 111 hairy roots, the plantlets were cultured hydroponically in Hoagland's solution at 50%
 112 concentration. The tubes were inserted with a hollow plastic straw to facilitate gas interchange
 113 and the supply of the solution, and were refilled every three/four days. The plants were placed

114 in a growing tent (1.5 m H x 1 m W x 1 m D) equipped with two blue 125 watts compact
115 fluorescent lamps (CFL) and a Sun Mate Grow CFL reflector. The photoperiod was adjusted
116 to a 10:14 hr light/darkness cycle (Conn *et al.*, 2006). The photosynthetic active radiation
117 (PAR) of 40 $\mu\text{mol photons m}^{-2} \text{s}^{-1}$ (30-45 $\mu\text{mol photons m}^{-2} \text{s}^{-1}$ is recommended) was measured
118 with a terrestrial quantum sensor LI-190SA and light meter LI-250A (Li-Cor International,
119 Ltd., UK). The tubes were covered individually with aluminium foil to prevent light damage
120 to the roots.

121 After 10 weeks, 48 plants (roots 8-10 cm length) in sets of 16 were placed on top of the
122 stainless-steel cages and transferred to 2.1 L tanks. The root biovolume was estimated by
123 rolling them into a plasticized sheet forming a cylinder, and the cylinder's volume was
124 calculated and recorded (Faulwetter *et al.*, 2013).

125 ***2.3.2 Synthetic filter media: two types of monofilament nonwoven plastic material***

126 The synthetic filtration media (polyamide nylon) consisted of two types of monofilament
127 nonwoven plastic material of different packing density. These synthetic media were tested to
128 compare their filtration removal efficiencies for *Microcystis* with that of the biofilters. The
129 plastic monofilament layers are bonded by heat to create a sheet of fabric. Differences in
130 flexibility that exist between fabric1 and fabric2 are based on the diameter of the filaments and
131 the number of filament layers that create the sheet of fabric. The filament diameter of fabric1
132 and fabric 2 is 0.5 and 0.03 mm respectively. Fabric1 is a two layered filament sheet of 0.8 mm
133 thickness and fabric2 is a multi-layered filament sheet of 1.8 mm thickness. Six stainless steel
134 cubic cages (10 cm³) were made to contain the fabrics, which were cut in squares of 10 cm²
135 (10 cm x 10 cm). Three cages used for fabric1 were tightly filled with 15 pieces each and
136 another three cages for fabric2 were filled with six squares each. The pieces were placed in the

137 cages with the largest surface area facing the direction of the flow. New cages were made and
138 fabric cut for each flow experiment.

139 **2.4 Photobioreactors for growing *Microcystis***

140 *Microcystis* was cultured in BG11 (modified by Ripka 1979). Aseptic techniques and
141 materials were used throughout the experiment. Four 150 cm³ sterile flasks each with 50 cm³
142 media were spiked with 1cm³ of the *Microcystis* stock culture and kept on the bench under
143 fluorescent laboratory lights providing photosynthetic active radiation (PAR) of 10 μmol
144 photons m⁻² s⁻¹ (recommended by the CCAP) (Imai *et al.*, 2008). The flasks were shaken
145 manually every three-four days and tested weekly for contamination prior to adding 10 cm³ of
146 fresh media, maintaining *Microcystis* at the exponential growth phase. An aliquot of 5 cm³ of
147 the *Microcystis* suspension was used as inoculum to grow larger quantities in photobioreactors.
148 The photobioreactors consisted of 1 L Duran bottles, placed in an open water bath with a
149 thermostat keeping the temperature at 22±1°C. The bottle mouth was closed with a sterile foam
150 plug covered with aluminium foil. To the initial volume of 300 cm³, 200-250 cm³ of BG11 was
151 added weekly up to 1 L. Air was diffused into the solutions at a rate of 0.1 – 0.4 L min⁻¹ with
152 a daily cycle (12:12 on/off) divided into four intervals. An additional fluorescent lamp provided
153 a range of 35 μmol photons m⁻² s⁻¹ to the closest photobioreactors and a minimum of 10 μmol
154 photons m⁻² s⁻¹ to the furthest, and the photoreactors were rotated weekly.

155 Quality control was conducted by assessing microscopic morphology of *Microcystis* cells
156 and conducting triplicates of cell counts from each bioreactor on a haemocytometer at x400
157 magnification using an inverted microscope (Imai *et al.*, 2008). *Microcystis* culture optical
158 density (O.D) was measured in triplicates at O.D₆₂₀ and O.D₇₅₀ nm (Vezie *et al.*, 2002; Dagnino
159 *et al.*, 2006) in a Shimadzu 1800-UV spectrophotometer. To ensure measurable changes in the

160 bioreactors, a minimum O.D₆₂₀ was estimated to be 0.3 (~6.5 x 10⁻⁶ cells cm³ ⁻¹) with the
161 resulting calibration Equation (2):

$$162 \quad Y=1E+07x + 504384 \quad (2)$$

163 To ensure there was no bacterial growth monitoring changes at O.D._{750nm} were conducted.

164 ***2.4.1 Microcystis as the particles in suspension***

165 *Microcystis* cells are spherical particles with an average size of 3.2 μm± 0.8μm (n=30),
166 obtained under light microscope (Eclipse E-200 Nikkon). Cells that were in division,
167 representing approximately 20% of the cell population, were also included in the average size.

168 An increase in the concentration of *Microcystis* cells is expected upstream of the filter
169 media (see Figure 1). The particle concentration in plug-flow mode can be expressed as a
170 dimensionless parameter, which represents the ratio of the particle concentration upstream of
171 the filter media relative to the inflow to the filtration unit following Equation (3),

$$172 \quad \text{Cumulative mass fraction (CMF)} = C_m/C_f \quad (3)$$

173 Where: CMF is the cumulative mass fraction; C_m is the concentration of cells on the
174 upstream side of the filter at sampling point A (figure 1) and C_f is the concentration of cells in
175 the inflow upstream of the filter unit at the inlet (figure 1). This parameter will indicate the
176 filtration mode of the filter media (US-EPA, 2005). Hence CMF =1 indicates an operating
177 system in deposition mode. The cells are moving with the inflowing water at a steady-rate
178 before passing through the filter media. CMF ≥1 indicates there is a scouring force applied
179 tangentially upstream to the media, and CMF ≤1 suggests the system operates in deposition
180 filtration mode.

181 **2.4.2 *Microcystis* cell count with flow cytometry**

182 *Microcystis* cell concentration was first estimated by manual counting on a
183 haemocytometer at x400 magnification on an inverted microscope. The large number of
184 samples generated and the poor count discrimination of low O.D readings (<0.015) led to the
185 use of flow cytometry for subsequent cell counts using a BD Accuri C6 (BD Biosciences, UK).

186 The fluidic system in the instrument is designed so that the suspended cells in the sample
187 are delivered one by one to a specific point with the illuminating beam. The velocity of the
188 samples loaded into the channel was set at 35 $\mu\text{l min}^{-1}$. The instrument measures the light
189 scattered by the cells at right angles to the laser beams (called side scatter, SS) and light
190 scattered in a forward direction (forward scatter, FS). The size and shape of the cells affects
191 the forward scatter whilst small structures (internal or external) of the cells affect more the SS.
192 The forward scatter threshold was set up to 15000 events, this mean that some debris and
193 instrument noise is ignored. The instrument is equipped with blue (488 nm) and red (638 nm)
194 excitation lasers and four emission filters (Table 2). The data were displayed using density dots
195 for two parameters using a bivariate histogram, or cytogram (C), where the dot density of a
196 population of cells forms a specific shape called a region (Dubelaar and Jonker, 2000). A region
197 can be drawn using a fluorescence parameter to define the population of interest (signature), or
198 a region can be used to limit the cells that are drawn on a light scatterplot (gate).

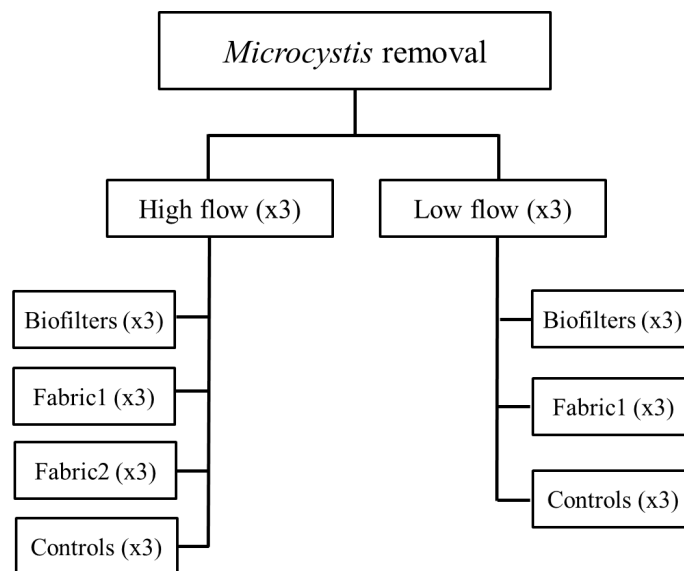
199 **Table 2. Naturally occurring fluorescent pigments in phytoplankton and their**
200 **detection on the BD Accuri C6.**

Pigments	Excitation	Emission	C6	Detector
Chlorophyll <i>a, b</i>	488	>640 nm	FL3 (670 LP)	
Phycoerythrin	488	575 nm	FL2 (585 \pm 20)	
Phycocyanin	640	650 nm	FL4 (675 \pm 12.5)	
Allophycocyanin	640	646 nm	FL4 (675 \pm 12.5)	

201 A manual gate was drawn around the cell population on a plot of chlorophyll-a
202 fluorescence (FL3; 488 nm excitation, 640 nm emission) versus phycocyanin fluorescence
203 (FL4; 640 nm excitation, 650 nm emission) and was used to discriminate and count the cells
204 against volume calibrated fluidics.

205 2.5 Testing the concept of *Microcystis* removal by biofilter roots.

206 To test for *Microcystis* cell removal by the biofilters (roots of living plants), the mesocosm
207 experiments were conducted under different continuous flow conditions. At high flow (54 ± 3.0
208 $\text{cm}^3 \text{min}^{-1}$) with biofilters and synthetic Fabric 1 and 2. Fabric2 had higher packing density
209 and was used as positive control with units as negative controls. At low flow ($1.3 \pm 0.2 \text{cm}^3$
210 min^{-1}) the design included biofilters, one type of synthetic fabric (fabric1) and negative
211 controls. The two flow conditions and three filter media treatment were each run in triplicates
212 (Figure 2).



214 **Figure 2. Schematic of the experimental mesocosm design at two flow conditions for**
215 **biofilters, synthetic fabrics (fabric 1 and 2) and controls (x3=triplicates).**

216 Prior to starting each of the experiments (high and low flow) the filtration units filled with
217 dechlorinated water and were left to stabilize for 2-3h (high flow) and 48h (low flow). The

218 outflow was calibrated to $54\pm 3.0 \text{ cm}^3 \text{ min}^{-1}$ and $1.3\pm 0.2 \text{ cm}^3 \text{ min}^{-1}$ for high and low flow
219 respectively. Replicates of the experiment were run for five, seven and 11 days, which
220 corresponded to two, three and approximately five hydraulic retention times. A 12w LED
221 submersible lamp with blue-red-white emission 400-700 nm, 800 lux providing approximately
222 $20.6 \mu\text{mol photons m}^{-2} \text{ s}^{-1}$ was introduced into the feed tank after being thoroughly disinfected
223 with 1 ppm chlorine solution and rinsed with sterilized (autoclaved) deionized water for the 11
224 day-run experiments. The high flow experiments ran for five hours.

225 Daily sampling (1 cm^3) was carried out for the low flow experiment at the sampling points
226 shown in Figure 1: feed tank (x3); sampling points A (x1), B (x3) (depths 1, 5 and 9 cm); and
227 C (x1) for each filtration unit. Samples were taken every 55 min from the feed tank (x3), A and
228 B (x1).

229 **2.5.1 Removal efficiency**

230 Removal efficiency as a percentage (RE%) was calculated for every paired inflow-outflow
231 sample taken from the filtration units. This parameter is calculated with the assumption of a
232 similar inlet and outlet flow rate, Equation (4)

$$233 \quad \%RE = \frac{(C_0 - C)}{C_0} \times 100 \quad (4)$$

234

235 where: C_0 is the concentration of *Microcystis* cells at the inlet and C is at the outlet.

236 **2.6 Data processing and statistical analysis**

237 Derived variables (ratio, percentages and rates) and exploratory statistical analysis were
238 undertaken using Excel (Microsoft © 2010) and SPSS v. 22 software. Data were transformed
239 to meet the normal distribution and other parametric assumptions, and if assumptions could not
240 be met, non-parametric tests were used. The non-parametric Friedman's test was applied to

241 find differences between treatments and the Wilcoxon-Sign-Rank test was applied to test for
242 differences in the number of *Microcystis* cells in the unit's inflow and outflow.

243 **2.7 Investigating chemical mechanisms: allelopathy**

244 Further experimental work was required to understand what quantitative and qualitative
245 mechanisms were taking place during the low flow experiments and determine if filtration
246 alone or in combination with allelopathy was contributing to the removal of cells in the
247 biofilters (Hilt and Gross, 2008; Rojo *et al.* 2013). Two composite root exudate samples (from
248 three biofilters) were screened and analysed using gas chromatography coupled with mass
249 spectrometry (GC-MS) to identify potential allelochemical compounds at Wessex Water
250 Scientific Centre, Bath, UK; a United Kingdom Accredited Systems laboratory.

251 **2.7.1 High pressure liquid chromatography: sample preparation and analysis**

252 To identify allelochemicals in the root exudate and root extraction from biofilters a new
253 method was developed using high pressure liquid chromatography (HPLC) at Wessex Water
254 Scientific Centre. Six chemical compounds (anthraquinone, gallic acid, gramine, hordenine, 4-
255 5 indole-aldehyde and stigmasterol) were purchased from Sigma-Aldrich. These compounds
256 are known to be produced by *Phalaris arundinacea* and were selected based on their
257 algaecide/algaostatic properties against cyanobacteria and micro-algae (Hong *et al.*, 2009; Xia
258 *et al.*, 2009; Shao *et al.*, 2013). The compounds were used as standards, and all the stock
259 solutions were prepared at 1 mg L⁻¹ concentration in methanol. Individual (1:100) and a mix
260 standard (6:100) in ultrapure water (UPW) solutions were prepared for extraction. Root
261 exudate samples of 100 cm³ taken from each biofilter were concentrated by a solid phase
262 extraction (SPE) step using a Visiprep (SupelcoTM – Sigma-Aldrich). Roots of three plants were
263 cut coarsely with a blender, adding 100 cm³ of 30% methanol in deionized water (MilliQPore
264 system) and concentrated by SPE. All samples were eluted from the cartridges with 1 cm³ of

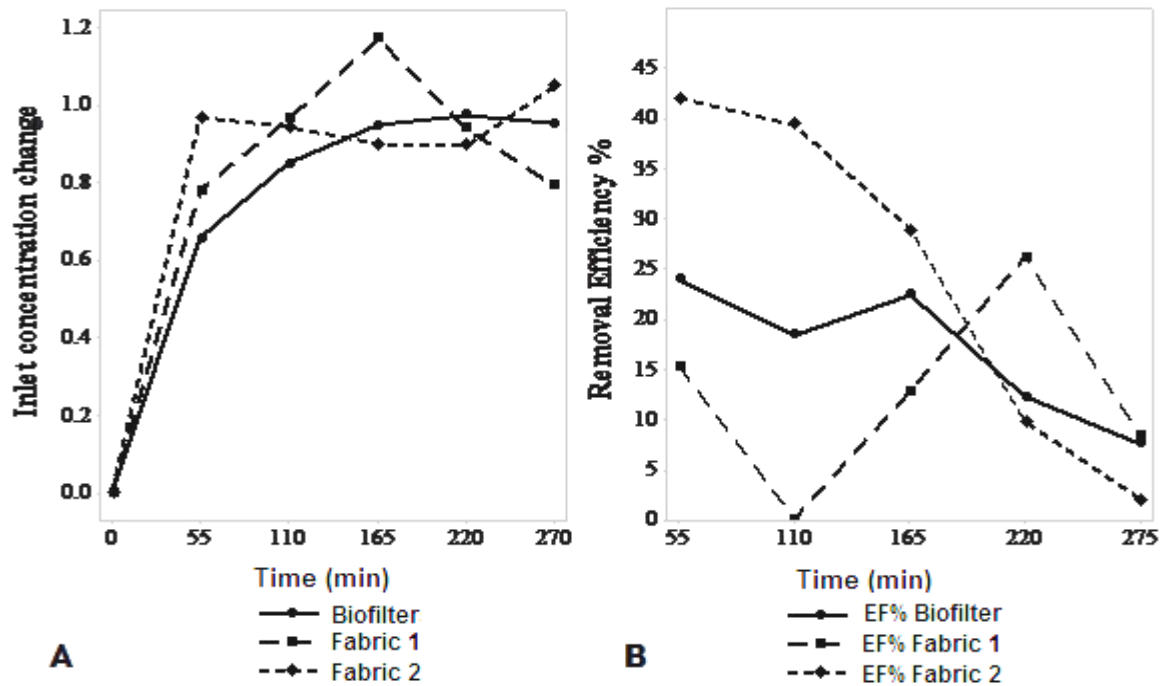
265 1% formic acid in methanol; the extracts were air dried (0.8 L min^{-1}) using a Visidry (Supelco
266 – Sigma-Aldrich); and the dried residue was resuspended with 1 cm^3 10% acetonitrile: 0.1 %
267 acetic acid in ultrapure water (UPW).

268 An Agilent 1200 LC series system was used with UV/Vis-DAD detector. A HPLC Agilent
269 column (C18, 150 mm x 5 mm) was used to achieve separation with a gradient elution
270 consisting of acidified (acetic acid) acetonitrile: acidified (acetic acid) water (95:5). Column
271 temperature was maintained at 40°C and total run time was 45 min. The UV/Vis absorbance
272 detector collected data at three wavelengths 205, 250 and 280 nm. Peak identity was validated
273 through the use of retention times of external non-extracted and extracted standards with their
274 respective spectrums All samples were kept at 5°C at all times.

275 **3. Results**

276 **3.1 *Microcystis* cell removal during high flow rate experiment**

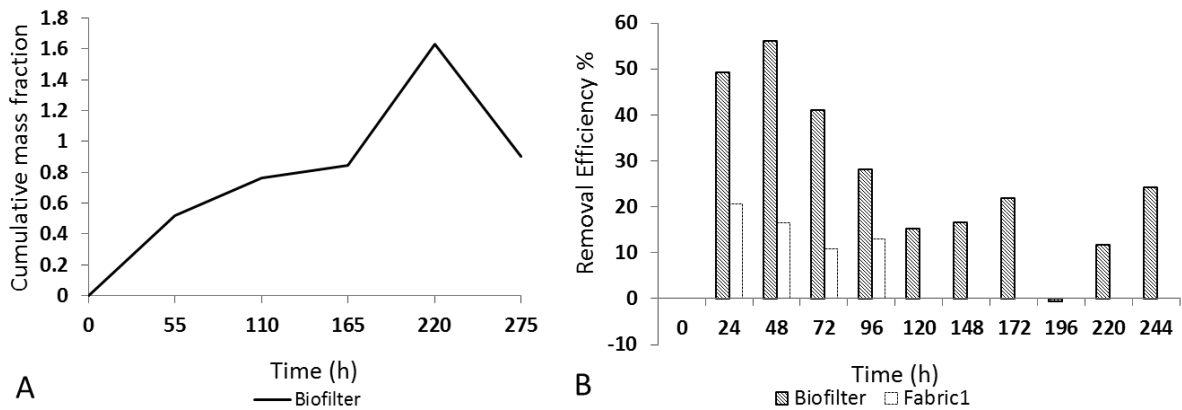
277 The packing densities of the synthetic filters with fibrous media were 0.03 for fabric1 and
278 0.07 for fabric2. The estimated packing density of the biofilters was 0.05. The cumulative mass
279 fraction of biofilters and fabric2 was ≤ 1 with the inflowing cell concentration, suggesting the
280 system operates in deposition filtration mode for both type of fibrous media (Figure 3-A). The
281 biofilter removal efficiency (RE%) of *Microcystis* cells is presented in Figure 3-B.



286 Microcystis cells were effectively removed from the biofilters and fabric2 (higher packing
 287 density) as shown by the decrease in numbers when comparing cell numbers from the outflow
 288 to the inflow (Wilcoxon-Sign Test $T=8$, $z=-4.34$, $p<0.5$, $r=-0.47$ for biofilter and $T=5$, $z=-0.46$,
 289 $p<0.5$, $r=-0.47$ for fabric2).

290 3.2 *Microcystis* cell removal during low flow rate experiments

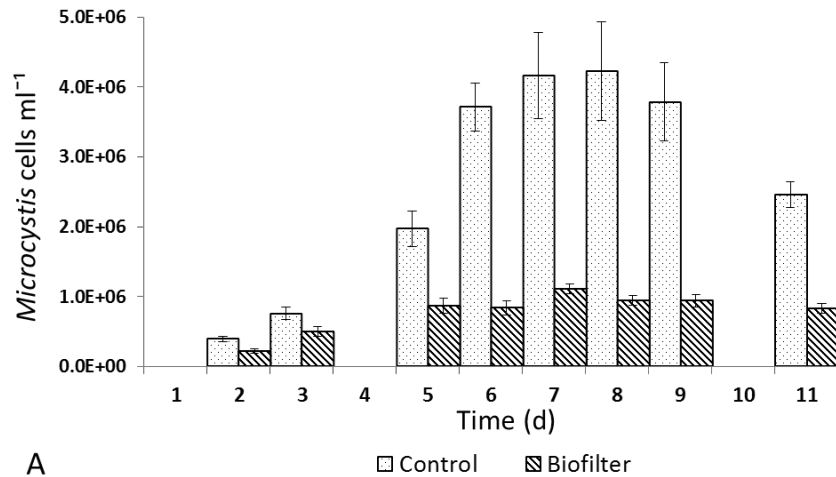
291 Results for *Microcystis* removal shown in Figure 4 correspond to the experimental run of
 292 five hydraulic retention time (5 HRT). The biofilter cumulative mass fraction was >1 at 4HRT
 293 before dropping rapidly (Figure 4A). Fabric1 results shown are from the run of 3HRT (Figure
 294 4-B). The biofilters showed removal efficiency of 40- 55% within the first three days, dropping
 295 to 10-20%; after three days RE for fabric1 was 8-20% (Figure 4-B).



297 **Figure 4-A. The cumulative mass fraction for the biofilters (solid line as a function**
 298 **of time (hours) equivalent to hydraulic retention time. 4-B Removal efficiency (%) of**
 299 ***Microcystis* cells by the biofilter in relation to time (hours).**

300 Colour change in the units with biofilters, fabric and the controls were observed. Results
 301 are shown for the biofilters and controls in Figure 5-A-B. The water in the biofilters is
 302 colourless, indicating the visual absence of *Microcystis* cells; while the fabric units and controls
 303 appear green, rich with cells. The same qualitative pattern was observed for all replicates of
 304 the experiment at low flow (run at 2 HRT and 3 HRT (x2)).

305 Quantification of *Microcystis* cells (by flow cytometry) was four and a half times higher
 306 in the controls and fabric1 (low packing density) when compared to the biofilters. The number
 307 of cells from the feed tank increased every 48-72 hours (results not shown) suggesting cell
 308 growth and conditions in the tank adequate for survival. By contrast the number of cells in the
 309 biofilters remained at $1 \times 10^6 \pm 2 \times 10^5 \text{ ml}^{-1}$ from day five onwards (Figure 5-A). Comparative
 310 results between controls and biofilters are considered only until day nine because a slight
 311 decline of *Microcystis* cells was observed in the controls after this day.



A



B.i

B.ii

313 **Figure 5-A. Quantitative changes in *Microcystis* average concentration (#cells ml⁻¹)**
 314 **for a mesocosm experiment run for 11 days or 5HRT. Controls (stippled), Biofilters**
 315 **(striped), number of samples is n=3 for each day. Error bars represent standard errors.**
 316 **5-B. Qualitative changes in colouration: green control units (B.i) indicating the presence**
 317 **of *Microcystis* cells versus colourless biofiltration units (B.ii).**

318 Significant differences in cell numbers were found between the inflow and outflow in the
 319 biofilters, with higher counts in the inflow than in the outflow (Wilcoxon sign-test $T=5$, $z=-$
 320 5.164 , $p<0.05$, $r=-0.53$). No significant differences in the number of *Microcystis* cells were
 321 found in the controls.

322 **3.3 Investigating chemical mechanisms of *Microcystis* removal by biofilters**

323 **3.3.1 Allelochemical presence and HPLC-UV/VIS-DAD**

324 Allelochemicals (i.e. phenols) and other secondary metabolites (i.e. cholesterol) were
325 found in the screened samples. Table 3 shows the identified compounds with the GC-MS
326 screening from the root exudate samples.

327 **Table 3. GC-MS screening results of water samples from the filter units**

Chemical	Concentration (ng dm ⁻³)
Stigmasterol	660
Phenols	620
Salicylates	440
Cholesterol	250
β-cyclocitral	220

328 Standards with their respective retention times from the developed method to identify
329 allelochemicals by HPLC-UV/Vis-DAD are shown in Table 4.

330 **Table 4. Limits of detection and quantification for the selected analytes.**

Analytes from standard solution	Limit of Detection (µg L ⁻¹)	Limit of Quantification (µg L ⁻¹)
Hordenine	3.63	11.01
Gramine	13.46	40.78
Naringin	9.11	38.86
4-nitroindole-5-carboxaldehyde	14.83	44.93
Anthraquinone	29.20	88.48

331

332 Table 5 compiles the identified compounds: gramine and 4-nitroindol-5-carboxaldehyde.

333 Hordenine could not be traced in the mixed standard sample.

334 **Table 5. Allelochemicals quantified in root exudates and root extracts (n=3).**

Allelochemicals	Root exudate mean±SE µg L⁻¹	Root extract mean±SE µg L⁻¹
Gramine		3447±1043
Naringin (ISTD 100 µg L ⁻¹)	109.3±9.9	4688±1433
4-Nitroindol-5-carboxaldehyde	96.13±10.1	176±10.1

335

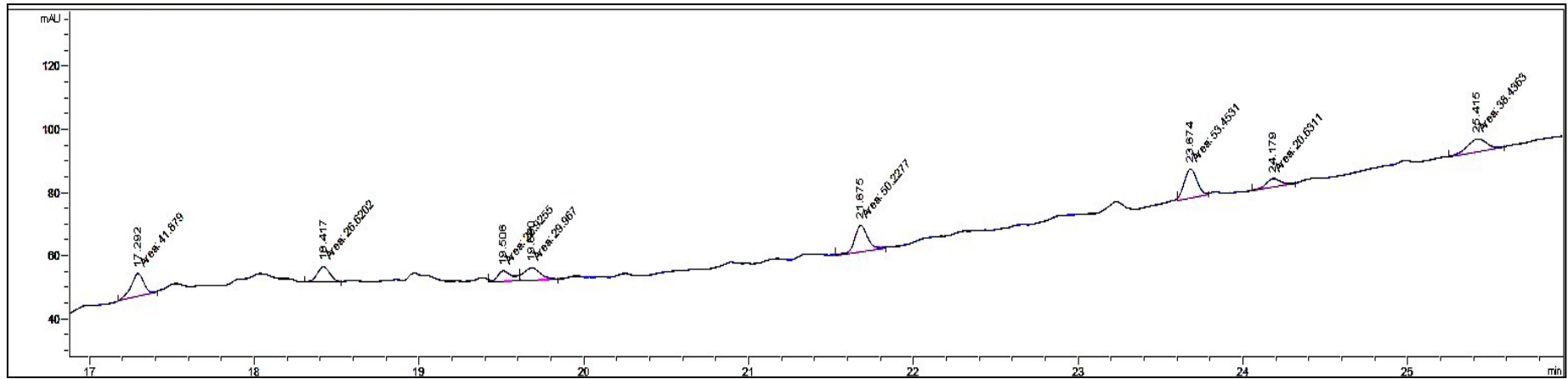
336 Figure 6 shows the chromatogram of a root exudate sample and root extracted sample.

337 There are a large number of unidentified compounds in the samples. Spectrums of the

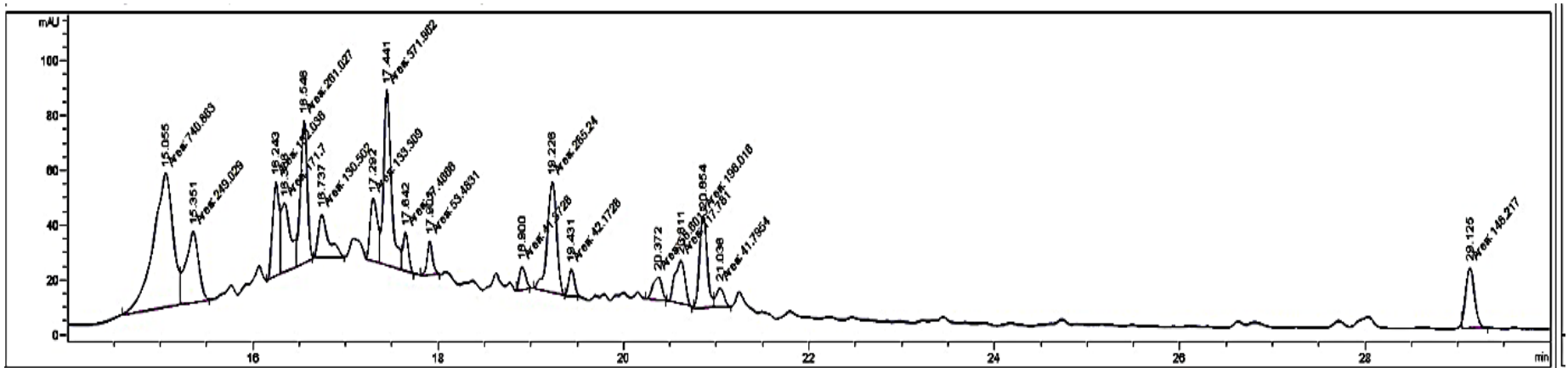
338 unidentified peaks and their retention times might be compatible with phenolic compounds.

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345 **4. Discussion**

346 *Microcystis* is a known bloom-forming cyanobacteria found worldwide in surface water
347 reservoirs, and there has been increasing interest in eco-biological/rhizofiltration systems for
348 its removal. The purpose of this study was to investigate whether *Microcystis* cells could be
349 removed by the roots of *Phalaris arundinacea* under continuous flows and to establish the
350 interactions between inflowing *Microcystis* cells with biofilters and synthetic filters. The
351 distribution of the cells/ compounds generated in the experimental system will are known to be
352 affected by hydrological processes (Alcocer *et al.*, 2012; Ruggeri and Sassi. 2013). Although
353 it is assumed a system will reach steady-state in hydraulic-biochemically mediated processes,
354 steady-state is rarely achieved in either plug-flow or continuously stirred systems (Poitier *et*
355 *al.*, 2005). At water or sewage treatment plants, where is very difficult to predict the load and
356 environmental changes, the system typically does not reach equilibrium (Davis and Conwell
357 2013). The system studied in this research did not reach steady-state within the experimental
358 period.

359 **4.1 *Microcystis* cells removal during the high flow experiment**

360 *Microcystis* cell behaviour (as suspended particles) in relation to natural and synthetic
361 media (natural and synthetic) suggests a deposition filtration mode or cumulative mass fraction
362 (CMF=1) (Figure 3-A). Differences in the cumulative mass fraction at different retention times
363 initially showed the cells through the biofilters reach CMF=1 at 220 min compared to fabric1,
364 where CMF=1 at 55 min. For removal efficiency, the biofilters were capable of removing 20 -
365 25 % of the *Microcystis* cells during three retention times. The most effective filter media was
366 fabric2 (synthetic filter with higher packing density than the biofilters and fabric1) with a
367 maximum removal efficiency (%) slightly above 40% compared to 25% for the biofilters and

368 to 17% for fabric 1 at 55 min. These results show that there is a physical removal mechanism of
369 the *Microcystis* cells by the biofilters, which can be related to packing density.

370 **4.2 *Microcystis* cell removal during the low flow experiment**

371 In the higher contact time experiment (i.e. low flow) the biofilters showed removal
372 efficiencies twice as high as those observed under high flow conditions, suggesting that the
373 increased exposure to the hydroponic rhizofiltration may contribute to higher removal
374 efficiencies. At lower flowrates, the cell numbers in the feed tank doubled between 48-72
375 hours, following a growth curve. A Growth Model fitted to the cell number data in the feed
376 tank explained 95% of the variance of the data (results not shown). This growth could also have
377 affected results for the CMF (Figure 4-A), as an increasing cell concentration would directly
378 affect the ratios. The number of cells in the controls $\geq 3.0 \times 10^6$ cells ml⁻¹, was at least twice as
379 high as in the biofilters where they did not increase above 1.2×10^6 cells ml⁻¹ (Figure 5-A).
380 Hence it was postulated that besides the physical removal chemical mechanisms may
381 contribute to the removal of *Microcystis* when exposed to biofilters i.e. rhizofiltration.

382 **4.2.2 *The role of the biofilters on Microcystis removal***

383 The most striking results found were the loss of colouration (bleaching) and the reduction
384 in cell number in the biofilters when compared to the control and fabric units. "Bleaching" or
385 chlorosis is defined in the literature as the change in pigmentation from blue-green to yellow-
386 green to yellow (or orange) (Collier and Grossman 1992; Baier *et al.*, 2014) in non-N₂ fixing
387 cyanobacteria (like *Microcystis*) under nitrogen starvation conditions. Chlorosis is a process
388 generally described after 72 hours of nitrogen starvation in cultures of cyanobacteria model
389 organisms such as *Synechocystis* and *Synechococcus* (Krasikov *et al. et al.*, 2012). However,
390 there is no reference in the literature to the chlorotic process as a complete lack of colouration
391 (clear as tap water) as observed in the biofilters (Figure 5). The chlorotic process of *Microcystis*

392 in the biofilters is observed after 72 hours, and at 96 hours there is a total absence of colouration
393 with no-absorbance spectrophotometric detection at O.D₆₂₀ and O.D₆₈₀ (results not shown).
394 Dagnino *et al.*, (2006) described a chlorotic process in nutrient-depleted *Microcystis* cultures
395 which after 3-5 days showed lack of colouration, but from blue-green to very pale blue-green
396 and decreasing cell density. They attributed this phenomenon to intercellular signalling present
397 in the medium of the nutrient-starved *Microcystis*. Intercellular signalling is a chemically
398 mediated process between microorganisms (e.g. cyanobacteria and algae/organisms of higher
399 taxa) known as allelopathy (Gross *et al.*, 2003). In this study, decrease in cell numbers was also
400 seen, measured and compared between the biofilters and the controls. These results suggest
401 that either nutrient competition between the roots in the biofilters and *Microcystis* cells or
402 allelochemical mechanisms with inhibiting/biocide effects (or both) induced chlorosis in the
403 *Microcystis* cells. It is important to point out that the *Microcystis* cells were continuously
404 injected to all the units in increasing concentration, but the only units with loss of colouration
405 or reduction in cell numbers were the biofilters.

406 **4.3 Investigating allelochemical in roots and root exudate**

407 The results of this study suggest the chlorotic effect and reduction in *Microcystis* cell
408 numbers in the biofilters could be triggered by allelopathy. Allelochemical compounds with
409 potentially algistatic/algaecide effects (Laue *et al.*, 2014) were identified in the root exudate at
410 nanogram concentrations (Table 2). These results mimic natural aquatic environments, where
411 the allelochemicals excreted by macrophytes are diluted in the surrounding water (Hilt and
412 Gross, 2008; Rojo *et al.*, 2013), but where they still have a suppression effect on phytoplankton
413 growth rates (Korner and Nicklisch, 2002; Mulderij *et al.*, 2007; Chang *et al.*, 2012). In water,
414 the distances between cells are crucial as the chemical information is transmitted by diffusion
415 and advective laminar flow (Wolfe 2000). By contrast, laboratory experiments are generally

416 carried out using *Microcystis* cells at concentrations of 1×10^5 - 1×10^6 μl in the presence of μg
417 or mg concentrations of allelochemicals either extracted from the roots or supplied
418 commercially to demonstrate their biocidal effect (Lurling *et al.*, 2013; Lurling and Van
419 Oosterhout 2014). However, allelopathy might not be only produced by the roots as any
420 bacteria and fungi present could be sources of allelopathic chemicals. Nevertheless, studies on
421 the detection and identification of allelochemicals in root tissue or root exudate from *Phalaris*
422 spp. let alone *Phalaris arundinacea*, have not been described in the literature.

423 The allelochemicals in the root exudate showed the presence of gramine and 4-nitroindol-
424 5-carboxaldehyde with the targeted method developed for allelochemical detection (Figure 6).
425 However, there were additional unidentified compounds present in the root exudate and a large
426 number in macerated root samples, which could potentially be released by the roots into the
427 water. It is envisaged in future experiments to increase the number of allelochemicals in the
428 mix-standard to enable further identification. However, this does not mean that all compounds
429 seen in the sample will have an algaecide/algistatic effect on *Microcystis*, and further
430 investigation will be required to distinguish the impact of individual compounds on *Microcystis*
431 cells.

432 **5. Conclusions**

433 *Microcystis* can be removed by the roots of *Phalaris arundinacea* under continuous
434 flow conditions, but the mechanism could vary depending on residence time and packing
435 density on synthetic/natural filter media. At higher residence times on natural filter media the
436 decrease in *Microcystis* cell numbers is accompanied by a chlorotic process, indicating
437 physicochemical mechanisms operate in natural filters compared to high flow where physical
438 deposition was the main removal mechanism. This highlights the importance of creating
439 pilot/field scale designs to allow low flow velocities and/or large retention times, and

440 increasing the probability of contact between the allelochemicals produced by the roots and the
441 *Microcystis* cells.

442 Overall, at low residence time, it was shown that the packing density of the filter porous
443 media plays the dominant role in *Microcystis aeruginosa* 1450/3 removal in both biofilters and
444 synthetic filter media. The packing density is a relevant factor to be considered in future Living-
445 Filter systems, if these are to be used as a pre-treatment process for phytoplankton removal.

446 Physicochemical interactions between living roots and *Microcystis* in hydroponic and
447 continuous flow conditions have not been described in the literature before. Findings from this
448 experimental set up are more realistic at demonstrating these physicochemical interactions
449 providing grounds for further experimentation, either with other phytoplankton or other plant
450 species. Additionally, the biofiltration set-up used in this study can be used to investigate and
451 optimize the removal of pharmaceuticals by living roots.

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